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# Mathematical Analysis of a Saint-Venant Model with Variable Temperature

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#### Abstract

We investigate the mathematical structure and properties of a Saint-Venant model with an energy equation and with temperature dependent transport coefficents. These equations model shallow water flows as well as thin viscous sheets over fluid substrates like oil slicks, atlantic waters in the Strait of Gilbraltar or float glasses. We exhibit an entropy function for the system of partial differential equations and by using the corresponding entropic variable we derive a symmetric conservative formulation of the system. The symmetrized Saint-Venant quasilinear system of partial differential equations is then shown to satisfy the nullspace invariance property and is recast into a normal form. Upon establishing the local dissipative structure of the linearuzed normal form, global existence results and asymptotic stability of equilibrium states are obtained. We finally derive the Saint-Venant equations with an energy equation taking into account the temperature dependence of transport coefficients from an asymptotic limit of a three-dimensional model.

## 1 Introduction

We investigate the derivation and mathematical properties of a viscous Saint-Venant system of partial differential equations with an energy equation and with temperature dependent transport coefficients. These equations model shallow water flows as well as thin viscous sheets over fluid substrates like oil slicks on water, surface atlantic waters above the denser Mediterranean sea in the Strait of Gilbraltar or float glasses used for the production of plate glass. Modeling temperature variations is important in various environmental and engineering applications or float glasses and this motivates the present study.

We first present the Saint-Venant system of partial differential equations with an energy equation and temperature dependent transport coefficients. We exhibit an entropy function for the system of partial differential equations and by using the corresponding entropic variable we derive a symmetric conservative formulation of the system. The symmetrizing variable is obtained from the entropy and not the kinetic energy as investigated by Tadmor [41], Hauke [18], and Carey [7] in the isothermal case. These symmetrized systems may also be useful for finite element discretization and numerical simulations [7, 18].

The symmetrized Saint-Venant system of partial differential equations is then shown to satisfy the nullspace invariance property and is recast into a normal form, that is, in the form of a symmetric hyperbolic-parabolic composite system. We next establish stability conditions of the source term as well as the local dissipative structure of the linearized normal system around constant equilibrium states. In particular the entropy production is nonnegative and the source term lies in the range of its derivative at equilibrium. Global existence results and asymptotic stability of equilibrium states are then obtained from Kawashima's theory of hyperbolic-parabolic systems [27] and its extension to systems with sources terms [16].

Numerous existence results can be found in the literature concerning the Saint-Venant system without an energy equation in various functional settings. We refer the reader notably to Serre [38] and Dafermos [9] for inviscid models, and Kanayama and Ushijima [24], Bernardi and Pironneau [5], Ton [42], Kloeden [29], Sundbye [40], Orenga [33], Lions [30], Bresch, Desjardins, and Métivier [6] and Wang and Xu [44] for viscous Saint-Venant models with a constant viscosity coefficient. To the authors' knowledge, it is the first time that the quasilinear Saint-Venant model with an energy equation and temperature dependent transport coefficients is investigated.

In the remaining part of the paper we derive the Saint-Venant equations with an energy equation taking into account the temperature dependence of transport coefficients. These equations are derived from an asymptotic study of a three dimensional incompressible model of a thin viscous sheet over a fluid substrate. The fluid substrate is incompressible and is modeled by using the hydrostatic approximation. We also derive typical free boundary conditions for the Saint-Venant model from the three dimensional governing equations and free boundary conditions associated with the viscous sheet.

Numerous derivations of the viscous Saint-Venant system of partial differential equations without an energy equation and with a constant viscosity can also be found in the literature. The inviscid equations were first written by Saint-Venant in 1871 [10]. Gerbeau and Perthame have revisited the derivation of the viscous case and validated the Saint-Venant model by a direct numerical comparison with the underlying incompressible model [13]. For viscous layers on a fluid substrate, Howell has derived a Saint-Venant model by performing an asymptotic analysis [20, 21]. Multilayer Saint-Venant models have recently been investigated by Audusse [1], Audusse and Bristeau [2], and Kanayama and Dan [26]. A Saint-Venant model with a temperature equations has been introduced by Benqué, Haugel, and Viollet [3] and used by Podsetchine, Schernewski, and Tejakusuma [36] to investigate the Oder Lagoon. The derivation of a Saint-Venant model of a thin viscous sheet over a fluid substrate with a temperature equation and taking into account the temperature dependence of transport coefficients as well as that of boundary conditions from an asymptotic analysis is new to the authors' knowledge.

## 2 Governing equations

We summatize in this section the Saint-Venant equations governing thin viscous sheets over fluid substrates as well as shallow water flows. We include an energy equation in the model since temperature variations are important in various engineering and environmental applications.

## 2.1 Conservation equations

The equations governing shallow water flows and thin viscous sheets over fluid substrates express the conservation of mass, horizontal momentum and energy. The mass conservation equation can be written in the form

$$\partial_t h + \partial_x (hu) + \partial_y (hv) = 0, \qquad (2.1)$$

where t denotes time, (x, y) the horizontal cartesian coordinates, h the height of the shallow water flow or of the viscous sheet in the vertical direction, u the velocity in the x direction, and v the velocity in the y direction. The momentum equations in the x and y directions can be written

$$\partial_t(hu) + \partial_x(hu^2 + p) + \partial_u(huv) + \partial_x\Pi_{xx} + \partial_u\Pi_{xy} = 0, \qquad (2.2)$$

$$\partial_t(hv) + \partial_x(huv) + \partial_y(hv^2 + p) + \partial_x\Pi_{yx} + \partial_y\Pi_{yy} = 0, \qquad (2.3)$$

where p is the kinematic pressure and  $\Pi_{xx}$ ,  $\Pi_{xy}$ ,  $\Pi_{yx}$ , and  $\Pi_{yy}$  are the coefficients of the kinematic viscous tensor  $\Pi$ . Finally the total energy conservation equation can be written in the form

$$\partial_t (he^{\text{tot}}) + \partial_x \big( (he^{\text{tot}} + p)u \big) + \partial_y \big( (he^{\text{tot}} + p)v \big) + \partial_x (\mathcal{Q}_x + \Pi_{xx}u + \Pi_{xy}v) + \partial_y (\mathcal{Q}_y + \Pi_{yx}u + \Pi_{yy}v) = \mathcal{H},$$
(2.4)

where  $e^{\text{tot}}$  is the total energy per unit mass,  $Q_x$ ,  $Q_y$  are the components of the kinematic heat flux Q, and  $\mathcal{H}$  denotes a heat loss term.

Since the Saint-Venant system of partial differential equations is naturally written in two dimensions, we will use in the following sections the indexing set  $C = \{x, y\}$  which is more explicit than the set  $C = \{1, 2\}$ .

#### 2.2 Thermodynamic properties

In the Saint-Venant system, the kinematic pressure is given by

$$p = \frac{1}{2}\alpha h^2, \tag{2.5}$$

where  $\alpha$  is a constant associated with gravity. On the other hand, the total energy per unit mass  $e^{\text{tot}}$  of the fluid sheet is given by

$$e^{\text{tot}}(h,T) = e + \frac{1}{2}(u^2 + v^2),$$
(2.6)

where e denotes the fluid sheet internal energy per unit mass. The internal energy e can be written

$$e(h,T) = e^{\text{st}} + \int_{T^{\text{st}}}^{T} c_v(\tau) d\tau + \frac{1}{2}\alpha h,$$
 (2.7)

where  $c_v$  is the heat capacity at constant volume per unit mass of the fluid, T the absolute temperature and  $e^{\text{st}}$  the formation energy of the fluid at the standard temperature  $T^{\text{st}}$ . We also define for convenience the formation energy at zero temperature  $e^0 = e^{\text{st}} - \int_0^{T^{\text{st}}} c_v(\tau) d\tau$  is such a way that the internal energy e can also be written  $e = e^0 + \int_0^T c_v(\tau) d\tau + \frac{1}{2}\alpha h$ . In comparison with the perfect gas model, we note that, with the Saint-Venant system modeling

In comparison with the perfect gas model, we note that, with the Saint-Venant system modeling fluid sheets, the height h plays the rôle of a density, the fluid is barotropic with a quadratic dependence of the pressure p on height h and the internal energy per unit mass of the fluid sheet e depends on both temperature T and height h.

The natural compatibility relation [30] between p and e is also satisfied since  $h^2 \partial_h e = p - T \partial_T p = \frac{1}{2} \alpha h^2$  so that there exists an entropy per unit mass s such that Gibbs relation T ds = de + pd(1/h) holds. From Gibbs relation, it is easily shown that  $T \partial_T s = \partial_T e = c_v$  and  $T \partial_h s = \partial_h e - p/h^2 = 0$  in such a way that

$$s = s^{\rm st} + \int_{T^{\rm st}}^{T} \frac{c_v(\tau)}{\tau} \, d\tau, \qquad (2.8)$$

where  $s^{\text{st}}$  is the formation entropy of the fluid at temperature  $T^{\text{st}}$ . The Gibbs function is further defined as g = e + p/h - Ts and will be required to express the entropic symmetrizing variable. Note finally that the Gibbs function g can be decomposed into  $g(h,T) = \bar{g}(T) + \alpha h$  where  $\bar{g}$  only depends on temperature and reads  $\bar{g} = e^{\text{st}} + \int_{T_{\text{st}}}^{T} c_v(\tau) d\tau - T(s^{\text{st}} + \int_{T_{\text{st}}}^{T} \frac{c_v(\tau)}{\tau} d\tau)$ .

**Remark 2.1.** Strictly speaking, denoting by  $\rho$  the—constant—density of the fluid, only the quantity  $\rho p/h$  is homogeneous to a pressure and p/h to a kinematic pressure. However, these h factors are natural since the equations are in two dimensions so that the internal constraints are transmitted through contact lines and not contact surfaces. Similarly, the quantity  $\rho eh$  is the internal energy per unit horizontal surface and  $\rho sh$  the entropy per unit horizontal surface of the fluid sheet.

## 2.3 Transport fluxes

The transport fluxes of the fluid sheet, that is, the kinematic viscous tensor  $\boldsymbol{\Pi}$  and the kinematic heat flux  $\boldsymbol{Q}$ , can be obtained from an asymptotic analysis as presented in Section 7. The kinematic viscous tensor is in the form.

$$\boldsymbol{\Pi} = -\nu h \Big( \boldsymbol{\partial}_{\boldsymbol{x}} \boldsymbol{v} + \boldsymbol{\partial}_{\boldsymbol{x}} \boldsymbol{v}^{t} + 2 \boldsymbol{\partial}_{\boldsymbol{x}} \cdot \boldsymbol{v} \boldsymbol{I} \Big),$$
(2.9)

where  $\partial_{\boldsymbol{x}}$  denotes the derivation vector  $\partial_{\boldsymbol{x}} = (\partial_x, \partial_y)^t$ ,  $\boldsymbol{v}$  the velocity vector  $\boldsymbol{v} = (u, v)^t$ ,  $\boldsymbol{x}$  the component  $\boldsymbol{x} = (x, y)^t$ ,  $\nu$  the kinematic shear viscosity of the fluid,  $\boldsymbol{I}$  the two dimensional unit tensor, and t the transposition operator. The viscous tensor  $\boldsymbol{\Pi}$  thus corresponds to the usual two dimensional formulation with a 'shear viscosity'  $h\nu$  and a 'volume viscosity'  $3h\nu$ . Upon decomposing the viscous tensor, we obtain

$$\boldsymbol{\Pi} = \begin{pmatrix} \Pi_{xx} & \Pi_{xy} \\ \Pi_{yx} & \Pi_{yy} \end{pmatrix} = -\nu h \begin{pmatrix} 2(2\partial_x u + \partial_y v) & \partial_y u + \partial_x v \\ \partial_y u + \partial_x v & 2(\partial_x u + 2\partial_y v) \end{pmatrix}.$$
(2.10)

We also define, for future use, the kinematic pressure tensor  $P = pI + \Pi$ , which can be interpreted as a kinematic momentum flux tensor. In addition, the kinematic heat flux is given by

$$\boldsymbol{Q} = (\mathcal{Q}_x, \mathcal{Q}_y)^t = -\varkappa h \partial_{\boldsymbol{x}} T, \qquad (2.11)$$

where  $\varkappa$  is the kinematic thermal conductivity of the fluid.

**Remark 2.2.** Strictly speaking, denoting by  $\rho$  the—constant—density of the fluid, only the quantity  $\rho \Pi/h$  is homogeneous to a viscous tensor and  $\Pi/h$  to a kinematic viscous tensor. Similarly, only the quantity  $\rho Q/h$  is homogeneous to a heat flux and Q/h to a kinematic heat flux. However, these h factors are natural since the internal constraints are transmitted through contact lines in two dimensional models. We have still termed  $\Pi$  the 'viscous tensor' and Q the 'heat flux' for the sake of simplicity. The quantities  $\eta = \nu \rho$  and  $\lambda = \varkappa \rho$  are the dynamic viscosity and the thermal conductivity, respectively, of the fluid.

**Remark 2.3.** Erroneous forms of the viscous terms are often found in the literature as for instance the forms  $-\partial_x \cdot (\nu(\partial_x(hv) + \partial_x(hv)^t + 2\partial_x \cdot (hv)I))$  or  $-h\partial_x \cdot (\nu(\partial_x v + \partial_x v^t + 2\partial_x \cdot vI))$  instead of the correct form obtained from asymptotics  $-\partial_x \cdot (\nu h(\partial_x v + \partial_x v^t + 2\partial_x \cdot vI))$ . Only the correct later form is energetically consistent as shown by Gent [12].

#### 2.4 Source terms

Heat exchanges are important in the modeling of shallow water flows [36] and various viscous sheets such that oil slicks and float glasses [20]. We consider a heat loss term in the form

$$\mathcal{H} = -\lambda^* (T - T^{\mathrm{e}}),$$

where  $T^{e}$  is a given constant ambiant temperature and  $\lambda^{*}$  a heat exchange coefficient.

**Remark 2.4.** Various other effects may be taken into account in the Saint-Venant system of partial differential equations depending on the particular application under consideration. For shallow water flows, it is possible for instance to take into account friction forces, wind effects, coriolis forces due to earth rotation and the sea depth [7, 13]. In the modeling of oil spills it is also important to take into account friction forces, water currents, shoreline deposition, winds effects and evaporation [34]. These extra source terms would not essentially modify the mathematical analysis that will be presented in the next sections.

**Remark 2.5.** Depending on the particular application under investigation, various terms may also be neglected in the Saint-Venant system of partial differential equations as for instance the kinetic energy terms in the energy conservation equation. However, these terms have been kept since they are important for structural purposes. They guarantee that the structure of the system is that of a symetrizable system of partial differential equations of hyperbolic-parabolic nature as will be shown in the next sections.

## 3 Quasilinear form

The governing equations presented in Section 2 are recast into a quasilinear vector form in this section.

#### 3.1 Conservative and natural variables

The conservative variable U associated with the equations (2.1)-(2.4) is given by

$$U = \left(h, hu, hv, he^{\text{tot}}\right)^{\tau},\tag{3.1}$$

and the natural variable Z by

$$Z = \left(h, u, v, T\right)^{t},\tag{3.2}$$

where h is the vertical height of the viscous sheet or of the shallow water flow playing the rôle of a density, u, v are the horizontal components of the mass averaged flow velocity in such a way that the velocity vector is  $\boldsymbol{v} = (u, v)^t$ ,  $e^{\text{tot}}$  is the total energy per unit mass of the fluid, t is the transposition symbol, and T is the absolute temperature.

The components of U naturally appear as conserved quantities in the Saint-Venant system with an energy equation. On the other hand, the components of the natural variable Z are more practical to use in actual calculations of differential identities.

## **3.2** Vector equations

The Saint-Venant equations modeling thin viscous sheet over fluid substrates or shallow water flows (2.1)-(2.4) can be rewritten into the compact form

$$\partial_t U + \partial_x F_x + \partial_y F_y + \partial_x F_x^{\text{dis}} + \partial_y F_y^{\text{dis}} = \Omega,$$
(3.3)

where  $\partial_t$  is the time derivative operator,  $\partial_x$ ,  $\partial_y$  are the space derivative operator in the x and y directions respectively,  $F_x$  and  $F_y$  are the convective flux in the x and y directions respectively,  $F_x^{\text{dis}}$  and  $F_y^{\text{dis}}$  are the dissipative flux in the x and y directions respectively, and  $\Omega$  is the source term. We will use the indexing set  $C = \{x, y\}$  in the following for the sake of simplicity.

From Section 2 the convective fluxes  $F_x$  and  $F_y$  in the x and y directions are given by

$$F_x = \left(hu, \, hu^2 + p, \, huv, \, he^{\text{tot}}u + pu\right)^t,\tag{3.4}$$

$$F_y = \left(hv, \, hvu, \, hv^2 + p, \, he^{\text{tot}}v + pv\right)^t,\tag{3.5}$$

where p is the pressure and  $e^{\text{tot}}$  the total energy per unit mass. The dissipative flux  $F_x^{\text{dis}}$  and  $F_y^{\text{dis}}$  in the x and y directions are

$$F_x^{\text{dis}} = (0, \Pi_{xx}, \Pi_{xy}, \mathcal{Q}_x + \Pi_{xx}u + \Pi_{xy}v)^t,$$
(3.6)

$$F_{y}^{\text{dis}} = \left(0, \, \Pi_{yx}, \, \Pi_{yy}, \, \mathcal{Q}_{y} + \Pi_{yx}u + \Pi_{yy}v\right)^{t}, \tag{3.7}$$

where  $\boldsymbol{\Pi}$  is the kinematic viscous stress tensor (2.9)(2.10) and  $\boldsymbol{Q}$  the kinematic heat flux vector (2.11). Finally, the source term is given by

$$\Omega = \left(0, 0, 0, \mathcal{H}\right)^t, \tag{3.8}$$

where  ${\cal H}$  is the heat loss term.

These equations have to be completed by the relations expressing the transport fluxes  $\Pi$  and Q, the thermodynamic properties p and  $e^{\text{tot}}$ , and the source term  $\Omega$ , already presented in Section 2. These relations have been given in terms of the natural variable and are used in the next sections to rewrite the system as a quasilinear system in terms of the conservative variable U.

#### **3.3** Mathematical assumptions

We describe in this section the mathematical assumptions concerning the thermodynamic properties and the transport coefficients associated with the Saint-Venant equations. These assumptions are assumed to hold in Sections 3, 4. and 5.

- (Th<sub>1</sub>) The fluid density  $\rho$  and the pressure factor  $\alpha$  are positive constants. The formation energy  $e^{\text{st}}$  and the formation entropy  $s^{\text{st}}$  are constants. The specific heat per unit mass  $c_v$ , is a  $C^{\infty}$  function of  $T \ge 0$  and there exist positive constants  $\underline{c}_v$  and  $\overline{c}_v$  with  $0 < \underline{c}_v \le c_v(T) \le \overline{c}_v$ , for  $T \ge 0$ .
- (Tr<sub>1</sub>) The kinematic shear viscosity  $\nu$ , the kinematic thermal conductivity  $\varkappa$ , and the thermal exchange coefficient  $\lambda^*$  are  $C^{\infty}$  functions of T for T > 0.
- (Tr<sub>2</sub>) The kinematic thermal conductivity  $\varkappa$ , the kinematic shear viscosity  $\nu$ , and the heat exchange coefficient  $\lambda^*$  are positive functions.

**Remark 3.1.** The adiabatic situation where  $\lambda^* = 0$  is also easily investigated and we only assume that  $\lambda^* > 0$  in order to simplify the formal presentation. Similarly, the situations where  $\nu$  and  $\varkappa$  are functions of both T and h are easily taken into account.

#### **3.4** Dissipation matrices and quasilinear system

In this section, we rewrite the system of partial differential equations (3.3) as a quasilinear system of second-order partial differential equations in terms of the conservative variable U. In order to express the natural variable Z in terms of the conservative variable U, we first investigate the map  $Z \to U$  and its range.

**Proposition 3.2.** The map  $Z \mapsto U$  is a  $C^{\infty}$  diffeomorphism from the open set  $\mathcal{O}_Z = (0, \infty) \times \mathbb{R}^2 \times (0, \infty)$  onto an open set  $\mathcal{O}_U$ . The open set  $\mathcal{O}_U$  is convex and given by

$$\mathcal{O}_U = \{ (u_1, u_2, u_3, u_4) \in \mathbb{R}^4; u_1 > 0, \quad u_4 - \phi(u_1, u_2, u_3) > 0 \},$$
(3.9)

where  $\phi: (0,\infty) \times \mathbb{R}^2 \to \mathbb{R}$  is defined by

$$\phi(u_1, u_2, u_3) = \frac{1}{2} \frac{u_2^2 + u_3^2}{u_1} + e^0 u_1 + \frac{1}{2} \alpha u_1^2,$$

and where  $e^0$  is the formation energy of the fluid at zero temperature.

*Proof.* From Assumption  $(\mathsf{Th}_1)$  and the expression of thermodynamic properties, we first deduce that the map  $Z \to U$  is  $C^{\infty}$  over the domain  $\mathcal{O}_Z$ . On the other hand, it is straightforward to show that the map  $Z \to U$  is one to one and that

$$\partial_Z U = \begin{pmatrix} 1 & 0 & 0 & 0 \\ u & h & 0 & 0 \\ v & 0 & h & 0 \\ e^{\rm tot} + \frac{1}{2} \alpha h & hu & hv & hc_v \end{pmatrix},$$

so that the matrix  $\partial_Z U$  is nonsingular over  $\mathcal{O}_Z$ . From the inverse function theorem, we deduce that  $Z \to U$  is a  $C^{\infty}$  diffeomorphism onto an open set  $\mathcal{O}_U$ . From  $he^{\text{tot}} = he + \frac{1}{2}h\boldsymbol{v}\cdot\boldsymbol{v}$ , the expressions of e, and  $(\mathsf{Th}_1)$ , it is then established that  $\mathcal{O}_U$  is given by (3.9). The convexity of  $\mathcal{O}_U$  is finally a consequence of the convexity of  $\phi$ , which is established by evaluating its second derivative. More specifically, for  $u_1 > 0$  and  $u_2, u_3 \in \mathbb{R}$ , we have

$$\begin{aligned} \partial_{u_1}^2 \phi &= \frac{u_2^2 + u_3^2}{u_1^3} + \alpha, \quad \partial_{u_1 u_2}^2 \phi = -\frac{u_2}{u_1^2}, \quad \partial_{u_1 u_3}^2 \phi = -\frac{u_3}{u_1^2}, \\ \partial_{u_2}^2 \phi &= \partial_{u_3}^2 \phi = \frac{1}{u_1}, \quad \partial_{u_2 u_3}^2 \phi = 0, \end{aligned}$$

in such a way that for any  $(x_1, x_2, x_3) \in \mathbb{R}^3$  we have

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$$\sum_{\leq i,j\leq 3} x_i x_j \partial_{u_i u_j}^2 \phi = \alpha x_1^2 + \frac{1}{u_1} \left( x_2 - \frac{u_2}{u_1} x_1 \right)^2 + \frac{1}{u_1} \left( x_3 - \frac{u_3}{u_1} x_1 \right)^2,$$

and the matrix  $(\partial^2_{u_i u_j} \phi)_{1 \le i,j \le 3}$  is positive definite over  $(0, \infty) \times \mathbb{R}^2$ .

In Section 2.3, the transport fluxes  $\boldsymbol{\Pi}$  and  $\boldsymbol{Q}$  and, therefore, the dissipative fluxes  $F_x^{\text{dis}}$  and  $F_y^{\text{dis}}$ , have been expressed in terms of the gradient of the natural variable Z. By using Proposition 3.2, these dissipation fluxes can thus be expressed as functions of the conservative variable gradients

$$F_i^{\rm dis} = -\sum_{j\in C} B_{ij}(U)\partial_j U,$$

where  $C = \{x, y\}$  and  $B_{ij}(U)$ ,  $i, j \in C$ , are the dissipation matrices. The matrix  $B_{ij}(U)$  is a square matrix of dimension 4, which relates the dissipative flux in direction *i* to the gradient of *U* in direction *j*.

We may further introduce the Jacobian matrices  $A_i, i \in C$ , of the convective fluxes  $F_i, i \in C$ , defined by

$$A_i = \partial_U F_i, \qquad i \in C$$

and finally rewrite the system (3.3) in the quasilinear form

$$\partial_t U + \sum_{i \in C} A_i(U) \partial_i U = \sum_{i,j \in C} \partial_i \left( B_{ij}(U) \partial_j U \right) + \Omega(U), \tag{3.10}$$

where the matrix coefficients are defined on the open convex set  $\mathcal{O}_U$ . As a direct consequence of  $(\mathsf{Th}_1)$  and  $(\mathsf{Tr}_1)$ , the system coefficients satisfy the following property  $(\mathsf{Edp}_1)$ 

(Edp<sub>1</sub>) The convective fluxes  $F_i$ ,  $i \in C$ , the dissipation matrices  $B_{ij}$ ,  $i, j \in C$ , and the source term  $\Omega$  are smooth functions of the variable  $U \in \mathcal{O}_U$ .

Expanding the sums over  $C = \{x, y\}$ , these equations can also be written in the more explicit form

$$\partial_t U + A_x(U)\partial_x U + A_y(U)\partial_y U = \partial_x \left( B_{xx}(U)\partial_x U \right) + \partial_x \left( B_{xy}(U)\partial_y U \right) + \partial_y \left( B_{yx}(U)\partial_x U \right) + \partial_y \left( B_{yy}(U)\partial_y U \right) + \Omega(U).$$
(3.11)

The detailed form of the coefficient matrices  $A_i(U)$ ,  $i \in C$ , and  $B_{ij}(U)$ ,  $i, j \in C$ , will not be needed in the following, and, therefore, will not be given.

## 4 Symmetrization of Saint-Venant equations

For hyperbolic systems of conservation laws, the existence of a conservative symmetric formulation has been shown to be equivalent to the existence of an entropy function [17, 11, 32]. These results have been generalized to the case of second order quasilinear systems of equations by Kawashima and Shizuta [28, 16, 14]. Kawashima and Shizuta [28] have also shown that, when the nullspace naturally associated with dissipation matrices is a fixed subspace, a symmetric system of conservation equations can be put into a normal form, that is, in the form of a symmetric hyperbolic-parabolic composite system. Giovangigli and Massot [16, 14]. have further characterized all possible normal forms for such systems.

In this section, we investigate the symmetrization of the Saint-Venant system with an energy equation (3.10). We exhibit a mathematical entropy function and derive the corresponding conservative symmetric form. This symmetric form is then used to derive a normal form. The symmetrizing variable is obtained from the entropy and not from the kinetic energy as investigated by Tadmor [41], Hauke [18], and Carey [7] in the isothermal case. The assumptions concerning thermodynamic properties  $(Th_1)$  and transport properties  $(Tr_1)(Tr_2)$  are assumed to hold in this section.

#### 4.1 Entropy and symmetric conservative form

The following definition of a symmetric (conservative) form for the system (3.10) is adapted from Kawashima and Shizuta [28, 16, 14].

**Definition 4.1.** Consider a  $C^{\infty}$  dipheomorphism  $U \to V$  from the open domain  $\mathcal{O}_U$  onto an open domain  $\mathcal{O}_V$  and consider the system in the V variable

$$\widetilde{A}_{0}(V)\partial_{t}V + \sum_{i\in C}\widetilde{A}_{i}(V)\partial_{i}V = \sum_{i,j\in C}\partial_{i}\left(\widetilde{B}_{ij}(V)\partial_{j}V\right) + \widetilde{\Omega}(V),$$

$$(4.1)$$

where

$$\begin{cases} \widetilde{A}_0 = \partial_V U, & \widetilde{A}_i = A_i \partial_V U = \partial_V F_i, \\ \widetilde{B}_{ij} = B_{ij} \partial_V U, & \widetilde{\Omega} = \Omega. \end{cases}$$

$$\tag{4.2}$$

The system is said of the symmetric form if the matrices  $\widetilde{A}_0$ ,  $\widetilde{A}_i$ ,  $i \in C$ , and  $\widetilde{B}_{ij}$ , i, jC, satisfy the following properties  $(S_1-S_4)$ .

- (S<sub>1</sub>) The matrix  $\widetilde{A}_0$  is symmetric positive definite for  $V \in \mathcal{O}_V$ .
- (S<sub>2</sub>) The matrices  $\widetilde{A}_i$ ,  $i \in C$ , are symmetric for  $V \in \mathcal{O}_V$ .
- (S<sub>3</sub>) We have  $\widetilde{B}_{ij}^t = \widetilde{B}_{ji}$  for  $i, j \in C$ , and  $V \in \mathcal{O}_V$ .
- (S<sub>4</sub>) The matrix  $\widetilde{B} = \sum_{i,j \in C} \widetilde{B}_{ij}(V) w_i w_j$  is symmetric and positive semidefinite, for  $V \in \mathcal{O}_V$  and  $w \in \Sigma^1$ , where  $\Sigma^1$  is the unit sphere in 2 dimensions.

The following generalized definition of a mathematical entropy function is adapted [16, 14] from Kawashima [27] and Kawashima and shizuta [28].

**Definition 4.2.** Consider a  $C^{\infty}$  function  $\sigma(U)$  defined over the open convex domain  $\mathcal{O}_U$ . The function  $\sigma$  is said to be an entropy function for the system (3.10) if the following properties hold.

- (E<sub>1</sub>) The function  $\sigma$  is a strictly convex function of  $U \in \mathcal{O}_U$  in the sense that the Hessian matrix  $\partial^2_U \sigma$  is positive definite over  $\mathcal{O}_U$ .
- (E<sub>2</sub>) There exists real-valued  $C^{\infty}$  functions  $q_i = q_i(U)$  such that

$$(\partial_U \sigma) A_i = \partial_U q_i, \quad i \in C, \quad U \in \mathcal{O}_U.$$

(E<sub>3</sub>) We have the property that, for any  $U \in \mathcal{O}_U$ 

$$\left(\partial_U^2 \sigma\right)^{-1} B_{ji}^t = B_{ij} \left(\partial_U^2 \sigma\right)^{-1}, \quad i, j \in C.$$

(E<sub>4</sub>) The matrix  $\widetilde{B} = \sum_{i,j\in C} B_{ij}(U) \left(\partial_U^2 \sigma(U)\right)^{-1} w_i w_j$  is symmetric positive semidefinite for any  $U \in \mathcal{O}_U$  and any  $w \in \Sigma^1$ .

Kawashima and Shizuta have established [28, 16, 14] the equivalence between conservative symmetrizability and the existence of an entropy function.

**Theorem 4.3.** The system (3.10) admits an entropy function  $\sigma$  defined over the open convex set  $\mathcal{O}_U$  if and only if it can be symmetrized over the open convex set  $\mathcal{O}_U$ . In this situation the symmetrizing variable V and the entropy function can be chosen such that

$$V = (\partial_U \sigma)^t. \tag{4.3}$$

As is usual for compressible gases [28], mixtures of reacting gases [16, 14], ambipolar plasmas [15], we define the mathematical entropy function  $\sigma$  of the Saint-Venant system with an energy equation as the opposite of the physical entropy hs

$$\sigma = -hs,$$

where s is the entropy per unit mass of the fluid under consideration (2.8). The mathematical entropy  $\sigma$  is associated with the physical entropy per unit surface hs and not the entropy per unit volume as usual. The corresponding entropic variable

$$V = \left(\partial_U \sigma\right)^t,$$

is then easily evaluated as

$$V = \frac{1}{T} \left( g - \frac{1}{2} \boldsymbol{v} \cdot \boldsymbol{v}, \, u, \, v, \, -1 \right)^t,$$

where g is the Gibbs function.

**Proposition 4.4.** The change of variable  $U \mapsto V$  is a  $C^{\infty}$  diffeomorphism from the open convex set  $\mathcal{O}_U$  onto an open set  $\mathcal{O}_V$ . The open set  $\mathcal{O}_V$  is given by

$$\mathcal{O}_V = \{ (u_1, u_2, u_3, u_4) \in \mathbb{R}^4; u_4 < 0, \quad u_1 - \psi(u_2, u_3, u_4) > 0 \},$$
(4.4)

where  $\psi : \mathbb{R}^2 \times (-\infty, 0) \to \mathbb{R}$  is given by

$$\psi(u_2, u_3, u_4) = -u_4 \overline{g}(-1/u_4) + \frac{1}{2} \frac{u_2^2 + u_3^2}{u_4},$$

and where the Gibbs function has been decomposed into  $g(h,T) = \overline{g}(T) + \alpha h$ .

Proof. From Proposition 3.2, the map  $Z \to U$  is a  $C^{\infty}$  diffeomorphism from  $\mathcal{O}_Z$  onto  $\mathcal{O}_U$ , so that we only have to show that the map  $Z \to V$  is a  $C^{\infty}$  diffeomorphism from  $\mathcal{O}_Z$  onto the open set  $\mathcal{O}_V$ . From Assumption (Th<sub>1</sub>) and the expression of thermodynamic properties, we first deduce that the map  $Z \to V$  is  $C^{\infty}$  over the domain  $\mathcal{O}_Z$ . It is then straightforward to show that the map  $Z \to V$  is one to one and that its range is  $\mathcal{O}_V$  since the Gibbs function can be decomposed in the form  $g(h, T) = \bar{g}(T) + \alpha h$ . In addition, the matrix  $\partial_Z V$  is easily shown to be nonsingular over  $\mathcal{O}_Z$  from its triangular structure and the proof is complete thanks to the inverse function theorem.

The conservative symmetric form is now investigated in the following theorem.

**Theorem 4.5.** The function  $\sigma$  is a mathematical entropy for the system (3.10), that is,  $\sigma$  satisfies Properties ( $E_1$ - $E_4$ ) of Definition 4.2. The symmetrized system associated with the entropic variable  $V \in \mathcal{O}_V$  can be written

$$\widetilde{A}_0 \partial_t V + \sum_{i \in C} \widetilde{A}_i \partial_i V = \sum_{i,j \in C} \partial_i \left( \widetilde{B}_{ij} \partial_j V \right) + \widetilde{\Omega}, \tag{4.5}$$

and satisfies Properties  $(S_1-S_4)$  of Definition 4.1. The matrix  $\widetilde{A}_0$  is given by

$$\widetilde{A}_0 = rac{T}{lpha} egin{pmatrix} 1 & Sym \ m{v} & m{v} \otimes m{v} + lpha h m{I} & \ e^{ ext{tot}} + rac{1}{2} lpha h & (e^{ ext{tot}} + rac{3}{2} lpha h) m{v}^t & \Upsilon_0 \end{pmatrix},$$

where

$$\Upsilon_0 = (e^{\text{tot}} + \frac{1}{2}\alpha h)^2 + \alpha h(u^2 + v^2 + Tc_v)$$

Since this matrix is symmetric, we only give its block lower triangular part and write "Sym" in the upper triangular part. Denoting by  $\boldsymbol{\xi} = (\xi_x, \xi_y)^t$  an arbitrary vector of  $\mathbb{R}^2$ , the matrices  $\widetilde{A}_i$ ,  $i \in C$ , are given by

$$\sum_{i\in C} \widetilde{A}_i \xi_i = \frac{T}{\alpha} \begin{pmatrix} \boldsymbol{v}\cdot\boldsymbol{\xi} & Sym \\ \boldsymbol{v}(\boldsymbol{v}\cdot\boldsymbol{\xi}) + \alpha h\boldsymbol{\xi} & \Sigma_{\boldsymbol{v},\boldsymbol{v}} \\ (e^{\text{tot}} + \frac{3}{2}\alpha h)\boldsymbol{v}\cdot\boldsymbol{\xi} & \Sigma_{e,\boldsymbol{v}} & \Upsilon_1 \boldsymbol{v}\cdot\boldsymbol{\xi} \end{pmatrix},$$

where

$$\Sigma_{\boldsymbol{v},\boldsymbol{v}} = \boldsymbol{v} \cdot \boldsymbol{\xi} \, \boldsymbol{v} \otimes \boldsymbol{v} + \alpha h(\boldsymbol{v} \otimes \boldsymbol{\xi} + \boldsymbol{\xi} \otimes \boldsymbol{v} + 2\boldsymbol{v} \cdot \boldsymbol{\xi} \, \boldsymbol{I}),$$
  

$$\Sigma_{e,\boldsymbol{v}} = (e^{\text{tot}} + \frac{5}{2}\alpha h)\boldsymbol{v} \cdot \boldsymbol{\xi} \, \boldsymbol{v}^t + (e^{\text{tot}} + \frac{1}{2}\alpha h)\alpha h \boldsymbol{\xi}^t,$$
  

$$\Gamma_1 = (e^{\text{tot}} + \frac{5}{2}\alpha h)(e^{\text{tot}} + \frac{1}{2}\alpha h) + \alpha h(u^2 + v^2 + Tc_v).$$

The dissipation matrices, are given by

$$\begin{split} \widetilde{B}_{xx} &= hT\nu \begin{pmatrix} 0 & 0 & 0 & 0 \\ 0 & 4 & 0 & 4u \\ 0 & 0 & 1 & v \\ 0 & 4u & v & \theta + 3u^2 \end{pmatrix}, \qquad \qquad \widetilde{B}_{xy} = hT\nu \begin{pmatrix} 0 & 0 & 0 & 0 \\ 0 & 0 & 2 & 2v \\ 0 & 1 & 0 & u \\ 0 & v & 2u & 3uv \end{pmatrix}, \\ \widetilde{B}_{yx} &= hT\nu \begin{pmatrix} 0 & 0 & 0 & 0 \\ 0 & 0 & 1 & v \\ 0 & 2 & 0 & 2u \\ 0 & 2v & u & 3uv \end{pmatrix}, \qquad \qquad \widetilde{B}_{yy} = hT\nu \begin{pmatrix} 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & u \\ 0 & 0 & 4 & 4v \\ 0 & u & 4v & \theta + 3v^2 \end{pmatrix}, \end{split}$$

where  $\theta = \varkappa T/\nu + (u^2 + v^2)$ . Denoting by  $\boldsymbol{\xi} = (\xi_x, \xi_y)^t$  and  $\boldsymbol{\zeta} = (\zeta_x, \zeta_y)^t$  arbitrary vectors of  $\mathbb{R}^2$ , we have

$$\sum_{i,j\in C} \widetilde{B}_{ij}\xi_i\zeta_j = hT\nu \begin{pmatrix} 0 & 0 & Sym \\ 0 & 2\boldsymbol{\xi}\otimes\boldsymbol{\zeta} + \boldsymbol{\zeta}\otimes\boldsymbol{\xi} + \boldsymbol{\xi}\cdot\boldsymbol{\zeta}\boldsymbol{I} \\ 0 & 2\boldsymbol{v}\cdot\boldsymbol{\zeta}\,\boldsymbol{\xi}^t + \boldsymbol{v}\cdot\boldsymbol{\xi}\,\boldsymbol{\zeta}^t + \boldsymbol{\zeta}\cdot\boldsymbol{\xi}\,\boldsymbol{v}^t & \theta\boldsymbol{\zeta}\cdot\boldsymbol{\xi} + 3\boldsymbol{v}\cdot\boldsymbol{\xi}\,\boldsymbol{v}\cdot\boldsymbol{\zeta} \end{pmatrix}$$

Finally, the source term  $\widetilde{\Omega}$  is given by

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$$\widetilde{\Omega} = \Omega$$

*Proof.* The calculation of the matrices  $\widetilde{A}_0$ ,  $\widetilde{A}_i$ ,  $i \in C$ , and  $\widetilde{B}_{ij}$ ,  $i, j \in C$ , is lengthy but straightforward and, therefore, is omitted. This calculation is easily conducted by using the natural variable Z as an intermediate variable. The symmetry properties of  $\widetilde{A}_0$ ,  $\widetilde{A}_i$ ,  $i \in C$ , and  $\widetilde{B}_{ij}$ ,  $i, j \in C$ , required in  $(S_1-S_4)$  are then obtained.

Consider then a vector  $\mathbf{x} \in \mathbb{R}^4$ , with components  $(\mathbf{x}_h, \mathbf{x}_u, \mathbf{x}_v, \mathbf{x}_T)^t$ . After a little algebra, we obtain

$$\mathcal{A}^{t}\widetilde{A}_{0}\mathsf{x} = \frac{T}{\alpha} \Big( \alpha h(\mathsf{x}_{u} + u\mathsf{x}_{T})^{2} + \alpha h(\mathsf{x}_{v} + v\mathsf{x}_{T})^{2} \\ + \big(\mathsf{x}_{h} + u\mathsf{x}_{u} + v\mathsf{x}_{v} + (e^{\mathrm{tot}} + \frac{1}{2}\alpha h)\mathsf{x}_{T}\big)^{2} + \alpha hc_{v}T\mathsf{x}_{T}^{2} \Big),$$

$$(4.6)$$

so that from  $(\mathsf{Th}_1)$  and the positivity of  $\alpha$ ,  $c_v$ , and T, we deduce that  $A_0$  is positive definite. Furthermore, a straightforward calculation leads to the following expression

$$\mathbf{x}^{t}\widetilde{B}(V, \boldsymbol{w})\mathbf{x} = T\nu h \Big( 3 \big( w_{x}(\mathbf{x}_{u} + u\mathbf{x}_{T}) + w_{y}(\mathbf{x}_{v} + v\mathbf{x}_{T}) \big)^{2} \\ + (\mathbf{x}_{u} + u\mathbf{x}_{T})^{2} + (\mathbf{x}_{v} + v\mathbf{x}_{T})^{2} + \frac{\varkappa}{\nu T} \mathbf{x}_{T}^{2} \Big),$$
(4.7)

where  $\mathbf{x} = (\mathbf{x}_h, \mathbf{x}_u, \mathbf{x}_v, \mathbf{x}_T)^t$  and  $w_x^2 + w_y^2 = 1$ . The matrix  $\tilde{B}$ —easily shown to be symmetric—is thus positive semidefinite from the positivity properties of transport coefficients. Finally,  $\sigma$  also satisfies  $(\mathsf{E}_1-\mathsf{E}_4)$  with  $q_x = \sigma u$  and  $q_y = \sigma v$ , as is easily checked and  $\sigma$  is strictly convex since  $\tilde{A}_0$  is positive definite over the open convex set  $\mathcal{O}_U$ .

We have thus established in this section that the Saint-Venant system satisfies the property

(Edp<sub>2</sub>) The quasilinear Saint-Venant system of partial differential equations (3.10) admits an entropy function  $\sigma$  on the open convex set  $\mathcal{O}_U$ .

## 4.2 Normal forms of Saint-Venant equations

The quasilinear Saint-Venant system of partial differential equations (3.10) has smooth coefficients and admits an entropy function, that is, satisfies the properties  $(\mathsf{Edp}_1)$  and  $(\mathsf{Edp}_2)$ . Introducing the symmetrizing variable  $V = (\partial_U \sigma)^t$ , the corresponding symmetric system (4.5) then satisfies Properties  $(\mathsf{S}_1-\mathsf{S}_4)$ . However, depending on the range of the dissipation matrices  $\tilde{B}$ , this system lies between the two limit cases of a hyperbolic system and a strongly parabolic system. In order to split the variables between hyperbolic and parabolic variables, we have to put the system into a normal form, in the form of a symmetric hyperbolic–parabolic composite system [27, 28, 16].

To this aim, introducing a new variable W, associated with a diffeomorphism  $V \to W$  from  $\mathcal{O}_V$ onto  $\mathcal{O}_W$ , changing of variable V = V(W) in (4.5) and multiplying on the left side by the transpose of the matrix  $\partial_W V$ , we get a new system in the variable W and have the following definition of a normal form [28].

**Definition 4.6.** Consider a system in symmetric form, as in Definition 4.1, and a diffeomorphism  $V \to W$  from the open set  $\mathcal{O}_V$  onto an open set  $\mathcal{O}_W$ . The system in the new variable W

$$\overline{A}_{0}(W)\partial_{t}W + \sum_{i \in C} \overline{A}_{i}(W)\partial_{i}W = \sum_{i,j \in C} \partial_{i} \left(\overline{B}(W)\partial_{j}W\right) + \overline{T}(W,\partial_{x}W) + \overline{\Omega}(W), \tag{4.8}$$

where

$$\begin{cases} \overline{A}_{0} = (\partial_{W}V)^{t} \widetilde{A}_{0} (\partial_{W}V), & \overline{B}_{ij} = (\partial_{W}V)^{t} \widetilde{B}_{ij} (\partial_{W}V), \\ \overline{A}_{i} = (\partial_{W}V)^{t} \widetilde{A}_{i} (\partial_{W}V), & \overline{\Omega} = (\partial_{W}V)^{t} \widetilde{\Omega}, \\ \overline{T} = -\sum_{i,j \in C} \partial_{i} (\partial_{W}V)^{t} \widetilde{B}_{ij} (\partial_{W}V) \partial_{j}W, \end{cases}$$

$$(4.9)$$

satisfies properties  $(S_1-S_4)$  rewritten in terms of overbar quantities. This system is then said to be of the normal form if there exists a partition of  $\{1, \ldots, 4\}$  into  $I = \{1, \ldots, n_0\}$  and  $II = \{n_0 + 1, \ldots, 4\}$ , such that the following properties hold.

(Nor<sub>1</sub>) The matrices  $\overline{A}_0$  and  $\overline{B}_{ij}$  have the block structure

$$\overline{A}_0 = \begin{pmatrix} \overline{A}_0^{I,I} & 0\\ 0 & \overline{A}_0^{II,II} \end{pmatrix}, \qquad \overline{B}_{ij} = \begin{pmatrix} 0 & 0\\ 0 & \overline{B}_{ij}^{II,II} \end{pmatrix}.$$

(Nor<sub>2</sub>) The matrix  $\overline{B}_{ij}^{II,II}(W,w) = \sum_{i,j\in C} \overline{B}_{ij}^{II,II}(W)w_iw_j$  is positive definite for  $W \in \mathcal{O}_W$  and  $w \in \Sigma^1$ . (Nor<sub>3</sub>) Denoting  $\partial_x = (\partial_x, \partial_y)^t$ , we have

$$\overline{\mathcal{T}}(W, \partial_{\boldsymbol{x}} W) = \left(\overline{\mathcal{T}}_{I}(W, \partial_{\boldsymbol{x}} W_{II}), \overline{\mathcal{T}}_{II}(W, \partial_{\boldsymbol{x}} W)\right)^{t}$$

where we have used the vector and matrix block structure induced by the partitioning of  $\{1, \ldots, 4\}$  into  $I = \{1, \ldots, n_0\}$  and  $II = \{n_0 + 1, \ldots, 4\}$ , so that we have  $W = (W_I, W_{II})^t$ , for instance.

A sufficient condition for system (4.1) to be recast into a normal form is that the nullspace naturally associated with dissipation matrices is a fixed subspace of  $\mathbb{R}^4$ . This is Condition N introduced by Kawashima and Shizuta. In the following lemma, we establish that the nullspace invariance property holds for the Saint-Venant system of partial differential equations.

**Proposition 4.7.** Let  $V \in \mathcal{O}_V$ ,  $\boldsymbol{w} = (w_x, w_y)^t \in \Sigma^1$ , and denote

$$\widetilde{B}(V, \boldsymbol{w}) = \sum_{i, j \in C} \widetilde{B}_{ij}(V) w_i w_j$$

The nullspace of the matrix  $\widetilde{B}$  is one-dimensional and given by

$$N(B) = \text{span}(1, 0, 0, 0)^t,$$

and we have  $\widetilde{B}_{ij}N(\widetilde{B}) = 0$ , for  $i, j \in C$ .

Proof. According to (4.7) the matrix  $\widetilde{B}$  is positive semidefinite, so that its nullspace is constituted by the vectors x of  $\mathbb{R}^4$  such that  $x^t \widetilde{B}x = 0$ . Denoting  $x = (x_h, x_u, x_v, x_T)^t$  and using (4.7), the null condition  $x^t \widetilde{B}x = 0$  implies that  $x_T = 0$  and  $x_u = x_v = 0$  and conversely. We have thus obtained that the nullspace of  $\widetilde{B}(V, \boldsymbol{w})$  is one-dimensional and spanned by  $(1, 0, 0, 0)^t$ , and it is thus independent of  $V \in \mathcal{O}_V$  and  $\boldsymbol{w} \in \Sigma^1$ . Finally, one easily checks that  $\widetilde{B}_{ij}(1, 0, 0, 0)^t = 0$ , for  $i, j \in C$ .

We have thus established the following property

(Edp<sub>3</sub>) The nullspace of the matrix  $\widetilde{B}(V, w) = \sum_{i,j \in C} \widetilde{B}_{ij}(V) w_i w_j$  does not depend on V and  $w \in \Sigma^1$ , dim $(N(\widetilde{B})) = 1$ , and we have  $\widetilde{B}_{ij}(V)N(\widetilde{B}) = 0$ ,  $i, j \in C$ .

We now investigate normal forms for the system (3.10), or, equivalently, for the system (4.5). Since the nullspace of the matrix  $\tilde{B}$  is spanned by the first canonical basis vector, the invertible matrix P of Lemma 3.7 of [16] can be taken to be the unit tensor in  $\mathbb{R}^{4,4}$  so that the auxiliary variables are simply U' = U and V' = V. Since  $U'_I = U_I = (h \text{ and } V'_{II} = V_{II} = (u, v, -1)/T$ , we obtain form the general characterization of normal form the following result.

**Theorem 4.8.** Any normal form of the system (4.1) is given by a change of variable in the form

$$W = \left(\phi_{I}(h), \phi_{II}\left(\frac{u}{T}, \frac{u}{T}, \frac{-1}{T}\right)\right)^{t},$$

where  $\phi_I$  and  $\phi_{II}$  are two diffeomorphisms of  $\mathbb{R}$  and  $\mathbb{R}^3$  respectively, and we have

$$\overline{\mathcal{T}}(W,\partial_x W) = \left(0, \,\overline{\mathcal{T}}_{II}(W,\partial_x W_{II})\right)^{T}$$

We can next use the possibility of mixing the parabolic components—the  $V'_{II} = V_{II}$  components established in Theorem 4.8, in order to simplify the analytic expression of the normal variable and, consequently, of the matrix coefficients appearing in the normal form. More specifically, we select the variable W = Z

$$W = \left(h, \, u, \, v, \, T\right)^{t},$$

easily obtained by combining the  $V'_{II} = V_{II}$  components and derive the corresponding normal form of the governing equations.

**Theorem 4.9.** The system in the variable  $W = (W_I, W_{II})^t$ , on the open convex set  $\mathcal{O}_W = (0, \infty) \times \mathbb{R}^2 \times (0, \infty)$ , with hyperbolic variable

 $W_I = h$ ,

and parabolic variable

$$W_{II} = \left(u, v, T\right)^t,$$

can be written in the form

$$\overline{A}_{0}^{I,I}\partial_{t}W_{I} + \sum_{i\in C}\overline{A}_{i}^{I,I}\partial_{i}W_{I} + \sum_{i\in C}\overline{A}_{i}^{I,II}\partial_{i}W_{II} = 0, \qquad (4.10)$$

$$\overline{A}_{0}^{II,II}\partial_{t}W_{II} + \sum_{i\in C}\overline{A}_{i}^{II,I}\partial_{i}W_{I} + \sum_{i\in C}\overline{A}_{i}^{II,II}\partial_{i}W_{II} = \sum_{i,j\in C}\partial_{i}\left(\overline{B}_{ij}^{II,II}\partial_{j}W_{II}\right) + \overline{\mathcal{T}}_{II} + \overline{\Omega}_{II}, \qquad (4.11)$$

and is of the normal form. The matrix  $\overline{A}_0$  is given by

$$\overline{A}_0 = \frac{1}{T} \begin{pmatrix} \alpha & 0 & 0\\ 0 & h \boldsymbol{I} & 0\\ 0 & 0 & \frac{h c_v}{T} \end{pmatrix},$$

Denoting by  $\boldsymbol{\xi} = (\xi_x, \xi_y)^t$  an arbitrary vector of  $\mathbb{R}^2$ , the matrices  $\overline{A}_x$  and  $\overline{A}_y$  are given by

$$\sum_{i \in C} \overline{A}_i \xi_i = \frac{1}{T} \begin{pmatrix} \alpha \boldsymbol{v} \cdot \boldsymbol{\xi} & Sym \\ \alpha h \boldsymbol{\xi} & h \boldsymbol{v} \cdot \boldsymbol{\xi} \boldsymbol{I} \\ 0 & 0 & \frac{h c_v}{T} \boldsymbol{v} \cdot \boldsymbol{\xi} \end{pmatrix}.$$
(4.12)

Denoting by  $\boldsymbol{\xi} = (\xi_x, \xi_y)^t$  and  $\boldsymbol{\zeta} = (\zeta_x, \zeta_y)^t$  arbitrary vectors of  $\mathbb{R}^2$ , the dissipation matrices,  $\overline{B}_{ij}$  are such that

$$\sum_{i,j\in C} \overline{B}_{ij}\xi_i\zeta_j = \frac{h}{T} \begin{pmatrix} 0 & Sym \\ 0_{2\times 1} & \nu(2\boldsymbol{\xi}\otimes\boldsymbol{\zeta} + \boldsymbol{\zeta}\otimes\boldsymbol{\xi} + \boldsymbol{\xi}\cdot\boldsymbol{\zeta}\boldsymbol{I}) & \\ 0 & 0_{1\times 2} & \frac{\varkappa}{T}\boldsymbol{\xi}\cdot\boldsymbol{\zeta}\boldsymbol{I} \end{pmatrix},$$

or equivalently

$$\overline{B}_{xx} = \frac{h}{T} \begin{pmatrix} 0 & 0 & 0 & 0 \\ 0 & 4\nu & 0 & 0 \\ 0 & 0 & \nu & 0 \\ 0 & 0 & 0 & \frac{\varkappa}{T} \end{pmatrix}, \qquad \qquad \overline{B}_{xy} = \frac{h}{T} \begin{pmatrix} 0 & 0 & 0 & 0 \\ 0 & \nu & 0 & 0 \\ 0 & \nu & 0 & 0 \\ 0 & 0 & 0 & 0 \end{pmatrix},$$
$$\overline{B}_{yx} = \frac{h}{T} \begin{pmatrix} 0 & 0 & 0 & 0 \\ 0 & \nu & 0 & 0 \\ 0 & 2\nu & 0 & 0 \\ 0 & 2\nu & 0 & 0 \\ 0 & 0 & 0 & 0 \end{pmatrix}, \qquad \qquad \overline{B}_{yy} = \frac{h}{T} \begin{pmatrix} 0 & 0 & 0 & 0 \\ 0 & \nu & 0 & 0 \\ 0 & 0 & 4\nu & 0 \\ 0 & 0 & 0 & \frac{\varkappa}{T} \end{pmatrix}$$

The term  $\overline{T}_{II}$  is easily evaluated as

$$\overline{\mathcal{T}}_{II} = -\frac{1}{T^2} \Big( 0, \, \boldsymbol{\Pi} \cdot \boldsymbol{\partial}_{\boldsymbol{x}} T, \, \boldsymbol{\Pi} : \boldsymbol{\partial}_{\boldsymbol{x}} \boldsymbol{v} + \boldsymbol{Q} \cdot \boldsymbol{\partial}_{\boldsymbol{x}} T \Big)^t,$$

whereas the source term  $\overline{\Omega} = (\overline{\Omega}_{I}, \overline{\Omega}_{II})^{t} = (\partial_{W}V)^{t} \Omega$  is given by

$$\overline{\Omega} = \left(0, 0, 0, -\frac{\lambda^*}{T^2}(T - T^{\rm e})\right)^t$$

*Proof.* The calculations are lengthy but straightforward and make use of Theorem 4.5 and Assumptions  $(Th_1)$ ,  $(Tr_1)$  and  $(Tr_2)$ .

## 5 Global existence for the Saint-Venant equations

In the previous sections, we have established that the quasilinear Saint-Venant system of partial differential equations is symmetrizable and can be written into a normal form so that we have already established the Properties ( $\mathsf{Edp}_1$ - $\mathsf{Edp}_3$ ). In this section we will first investigate the existence of constant equilibrium states or Property ( $\mathsf{Edp}_4$ ). We will next investigate the corresponding linearized normal form and linearized source term. We will indeed establish the local dissipativity properties labeled ( $\mathsf{Dis}_1$ - $\mathsf{Dis}_4$ ) that will insure the asymptotic stability of equilibrium states [16, 14]. In particular, global existence of solution around equilibrium states as well as decrease estimates will be obtained for the quasilinear Saint-Venant system with a temperature equation. We will use the normal variable W = Zintroduced in Theorem 4.9 but other normal variables could be used as well.

## 5.1 Local dissipative structure

We remind that the source term  $\Omega$  is given by  $\Omega = (0, 0, 0, -\lambda^*(T - T^e))^t$ , where  $\lambda^*$  is a positive coefficient and  $T^e > 0$  a positive temperature.

**Proposition 5.1.** Let a height  $h^e > 0$  and a velocity  $v^e = (u^e, v^e)^t \in \mathbb{R}^2$  be given. Then the state  $U^e$  defined by

$$U^{\mathrm{e}} = \left(h^{\mathrm{e}}, h^{\mathrm{e}}u^{\mathrm{e}}, h^{\mathrm{e}}v^{\mathrm{e}}, h^{\mathrm{e}}e^{\mathrm{tot}}(h^{\mathrm{e}}, T^{\mathrm{e}})\right)^{t},$$

is an equilibirum state

 $\Omega(U^{\rm e}) = 0,$ 

and for this constant stationary state we also have  $Z^{e} = (h^{e}, u^{e}, v^{e}, T^{e})^{t}$ .

Selecting arbitrarily  $Z^{e} = (h^{e}, u^{e}, v^{e}, T^{e})^{t}$  we have established the following property

(Edp<sub>4</sub>) There exists a constant equilibrium state  $U^{e}$  such that  $\Omega(U^{e}) = 0$ .

We will denote by  $V^{e}$  and  $W^{e}$  the equilibrium states in the variables V and W, respectively. In order to establish a global existence theorem, we further need to investigate the local dissipative structure of the source term.

**Proposition 5.2.** The linearized source term  $\widetilde{L}(V^{e}) = -(\partial_{V}\widetilde{\Omega})(V^{e})$  at the stationary state  $V^{e}$  constructed in Proposition 5.1 is given by

where  $\lambda^{*e} = \lambda^{*}(T^{e})$ . This matrix  $\widetilde{L}(V^{e})$  is symmetric positive semidefinite and satisfies

$$R(\tilde{L}(V^{\mathrm{e}})) = \operatorname{span}(0, 0, 0, 1)^{t},$$

in such a way that we have  $\Omega(U(V)) = \widetilde{\Omega}(V) \in R(\widetilde{L}(V^e))$  for all  $V \in \mathcal{O}_V$ .

*Proof.* Evaluating the matrix  $\widetilde{L}(V^{e})$  is straightforward,  $\widetilde{L}(V^{e})$  is positive semidefinite, and obviously  $R(\widetilde{L}(V^{e})) = \operatorname{span}(0,0,0,1)^{t}$ .

**Proposition 5.3.** Let  $U^{e} = U(Z^{e})$  with  $Z^{e} = (h^{e}, u^{e}, v^{e}, T^{e})^{t}$  be a constant equilibrium state in  $\mathcal{O}_{U}$  constructed as in Proposition 5.1. Then there exists a neighborhood  $\mathfrak{V}$  of  $V^{e}$  and a positive constant  $\delta$  such that

$$\delta | \widetilde{\Omega}(V) |^2 \leq -\langle V - V^{\mathrm{e}}, \widetilde{\Omega}(V) \rangle, \qquad V \in \mathfrak{V}.$$
(5.2)

*Proof.* From the expression of V, we obtain

$$\langle V - V^{\mathrm{e}}, \widetilde{\Omega}(V) \rangle = -\frac{\lambda^{*}}{TT^{\mathrm{e}}} (T - T^{\mathrm{e}})^{2},$$

and (5.2) since  $|\widetilde{\Omega}(V)|^2 = \lambda^{*2}(T - T^e)^2$  and  $\lambda^*$  is a positive function.

We have thus established the Properties  $(\mathsf{Dis}_3)$  and  $(\mathsf{Dis}_4)$ 

- (Dis<sub>3</sub>) The smallest linear subspace containing the source term vector  $\widetilde{\Omega}(V)$ , for all  $V \in \mathcal{O}_V$ , is included in the range of  $\widetilde{L}(V^{*e})$ , with  $\widetilde{L} = (\partial_V W)^t \overline{L}(V^{*e}) \partial_V W$ .
- (Dis<sub>4</sub>) There exists a neighborhood of  $V^{*e}$ , in  $\mathcal{O}_V$ , and a positive constant  $\delta > 0$  such that, for any V in this neighborhood, we have

$$\delta |\widetilde{\Omega}(V)|^2 \le -\langle V - V^{*e}, \widetilde{\Omega}(V) \rangle.$$

## 5.2 Linearized normal form

If we linearize the symmetric hyperbolic-parabolic system (4.10)(4.11) around a constant stationary state  $W^{e} = (h^{e}, u^{e}, v^{e}, T^{e})^{t}$ , we obtain the linear symmetric system

$$\overline{A}_{0}(W^{\mathrm{e}})\partial_{t}z + \sum_{i \in C} \overline{A}_{i}(W^{\mathrm{e}})\partial_{i}z = \sum_{i,j \in C} \overline{B}_{ij}(W^{\mathrm{e}})\partial_{i}\partial_{j}z - \overline{L}(W^{\mathrm{e}})z,$$
(5.3)

where the zeroth order term is defined as  $\overline{L}(W^{e}) = -(\partial_{W}\overline{\Omega})(W^{e})$  and is given by

Taking into account that (4.10)(4.11) is a normal form, and since the matrix  $\overline{L}(W^e)$  is symmetric positive semi-definite, we obtain that Property  $(\mathsf{Dis}_1)$  is satisfied

(**Dis**<sub>1</sub>) The matrix  $\overline{A}_0(W^{\text{e}})$  is symmetric positive definite, the matrices  $\overline{A}_i(W^{\text{e}})$ ,  $i \in C$ , are symmetric, we have the reciprocity relations  $(\overline{B}_{ij}(W^{\text{e}}))^t = \overline{B}_{ji}(W^{\text{e}})$ ,  $i, j \in C$ , and the matrix  $\overline{L}(W^{\text{e}})$  is symmetric positive semidefinite.

We next have to investigate the existence of compensating matrices  $K^j$ ,  $j \in C$  [27, 39, 16]. In the following proposition, we denote by  $\overline{B}(W^{e}, \boldsymbol{\xi})$  the matrix  $\overline{B}(W^{e}, \boldsymbol{\xi}) = \sum_{i,j \in C} \overline{B}_{ij} \xi_{i} \xi_{j}$ .

**Proposition 5.4.** For a sufficiently small and positive a, the matrices  $K^{j}, j \in C$ , defined by

$$\sum_{j \in C} \xi_j K^j = a \begin{pmatrix} 0 & \boldsymbol{\xi}^t & 0 \\ -\boldsymbol{\xi} & 0_{2\times 2} & 0_{2\times 1} \\ 0 & 0_{1\times 2} & 0 \end{pmatrix} \overline{A}_0 (W^{\mathrm{e}})^{-1},$$

where  $\boldsymbol{\xi} = (\xi_x, \xi_y)^t$ , are compensating matrices. In particular, the products  $K^j \overline{A}_0(W^e)$  are skew-symmetric and the matrix

$$\sum_{i,j\in C} K^{j}\overline{A}_{i}(W^{\mathrm{e}})\xi_{i}\xi_{j} + \overline{B}(W^{\mathrm{e}},\boldsymbol{\xi}),$$

is positive definite for  $\boldsymbol{\xi} \in \Sigma^1$ .

*Proof.* It is obvious by construction that the products  $K^j \overline{A}_0(W^e)$ ,  $j \in C$ , are skew-symmetric. On the other hand, a direct calculation yields

$$\sum_{i,j\in C} \xi_j K^j \overline{A}_i(W^{\mathbf{e}}) \xi_i = a \begin{pmatrix} \alpha |\boldsymbol{\xi}|^2 & (\boldsymbol{v}^{\mathbf{e}} \cdot \boldsymbol{\xi}) \boldsymbol{\xi}^t & 0\\ -(\boldsymbol{v}^{\mathbf{e}} \cdot \boldsymbol{\xi}) \boldsymbol{\xi} & -h^{\mathbf{e}} \boldsymbol{\xi} \otimes \boldsymbol{\xi} & 0_{2\times 1}\\ 0 & 0_{1\times 2} & 0 \end{pmatrix}$$
(5.5)

where the superscript <sup>e</sup> indicates that the corresponding quantity is evaluated at  $W^{e}$ . As a consequence, for  $\boldsymbol{\xi} \in \Sigma^{1}$ , and  $x = (x_{h}, x_{u}, x_{v}, x_{T})^{t}$ , we have  $|\boldsymbol{\xi}| = 1$ , and there exists  $\beta > 0$  such that

$$\langle x^t, \sum_{i,j\in C} \xi_j K^j \overline{A}_i(W^e) \xi_i x \rangle \geq \frac{a\alpha}{2} \left( x_h^2 - \beta (x_u^2 + x_v^2 + x_T^2) \right).$$

Using now Property  $(Nor_2)$ , the matrix

$$\sum_{i,j\in C} K^j \overline{A}_i(W^{\mathrm{e}}) \xi_i \xi_j + \overline{B}(W^{\mathrm{e}}, \boldsymbol{\xi})$$

is positive definite for  $\boldsymbol{\xi} \in \Sigma^1$  and a sufficiently small.

We have thus established  $(Dis_2)$ 

(Dis<sub>2</sub>) The linearized system is strictly dissipative in the sense that there exists compensating matrices  $K^j, j \in C$ .

**Remark 5.5.** Different formulations can be used in order to establish the strict dissipativity of the linearized normal form as detailed in [39]. However, we have chosen to directly establish the stronger Proposition 5.4 which implies the existence of a combined compensating matrix  $K = \sum_{j \in C} K^j \xi_j$  as discussed by Shizuta and Kawashima [39].

## 5.3 Global existence and asymptotic stability

In the previous sections, we have established that Properties  $(\mathsf{Edp}_1-\mathsf{Edp}_4)$  and  $(\mathsf{Dis}_1-\mathsf{Dis}_4)$  are satisfied. Therefore the existence theorems established in References [16, 14] can be applied to the system (4.10)(4.11) governing shallow water flows or thin viscous sheets over fluid substrates written in the  $W = (W_I, W_{II})^t$  variable, with the hyperbolic variable

$$W_I = h$$

and the parabolic variable

$$W_{II} = (u, v, T)^{\iota}.$$

**Theorem 5.6.** Consider the system (4.10)(4.11) with d = 2,  $l \ge \lfloor d/2 \rfloor + 2$ , and let  $W^0(x)$  be such that

$$W^0 - W^e \in W_2^l(\mathbb{R}^d).$$

Then, if  $\|W^0 - W^e\|_{l,2}$  is small enough, there exists a unique global solution to the the Cauchy problem (4.10)(4.11)

$$\overline{A}_0 \partial_t W + \sum_{i \in C} \overline{A}_i \partial_i W = \sum_{i,j \in C} \partial_i \left( \overline{B}_{ij} \partial_j W \right) + \overline{\mathcal{T}} + \overline{\Omega}$$

with initial condition

$$W(0,x) = W^0(x),$$

such that

$$W_{I} - W_{I}^{e} \in C^{0}([0,\infty); W_{2}^{l}(\mathbb{R}^{d})) \cap C^{1}([0,\infty); W_{2}^{l-1}(\mathbb{R}^{d})),$$
  

$$W_{II} - W_{II}^{e} \in C^{0}([0,\infty); W_{2}^{l}(\mathbb{R}^{d})) \cap C^{1}([0,\infty); W_{2}^{l-2}(\mathbb{R}^{d})),$$
(5.6)

and

$$\begin{cases} \partial_{\boldsymbol{x}} W_{\boldsymbol{I}} \in \quad L^2(0,\infty;W_2^{l-1}(\mathbb{R}^d)), \\ \partial_{\boldsymbol{x}} W_{\boldsymbol{I}\boldsymbol{I}} \in \quad L^2(0,\infty;W_2^l(\mathbb{R}^d)). \end{cases}$$

Furthermore, W satisfies the estimate

$$\|W(t) - W^{e}\|_{l,2}^{2} + \int_{0}^{t} \left( \|\partial_{\boldsymbol{x}} h(\tau)\|_{l-1,2}^{2} + \|\partial_{\boldsymbol{x}} u(\tau)\|_{l,2}^{2} + \|\partial_{\boldsymbol{x}} v(\tau)\|_{l,2}^{2} + \|\partial_{\boldsymbol{x}} T(\tau)\|_{l,2}^{2} \right) d\tau \leq \beta \|W^{0} - W^{e}\|_{l,2}^{2},$$
(5.7)

where  $\beta$  is a positive constant and  $\sup_{x \in \mathbb{R}^d} |W(t) - W^e|$  goes to zero as  $t \to \infty$ .

**Theorem 5.7.** Keeping the assumptions of the preceding theorem, assume that d = 2,  $l \ge [d/2] + 3$ and  $W^0 - W^e \in W_2^l(\mathbb{R}^d) \cap L^p(\mathbb{R}^d)$  with  $p \in [1, 2)$ . Then, if  $||W(t) - W^e||_{l-2, 2} + ||W(t) - W^e||_{0, p}$  is small enough, the unique global solution to the Cauchy problem satisfies for  $t \in [0, \infty)$  the decay estimate

$$\|W(t) - W^{\mathbf{e}}\|_{l-2,2} \le \beta (1+t)^{-\gamma} \Big( \|W(t) - W^{\mathbf{e}}\|_{l-2,2} + \|W(t) - W^{\mathbf{e}}\|_{0,p} \Big),$$

where  $\beta$  is a positive constant and  $\gamma = d \times (1/2p - 1/4)$ .

**Remark 5.8.** Theorems 5.6 and 5.7 are easily adapted to the situation d = 1, further assuming that p = 1, or to the situation  $\lambda^{*e} = 0$  where  $T^{e}$  can then be chosen arbitrarily. Various extra effects like friction forces or winds effects can also easily be taken into account in Theorem 5.6.

## 6 A thin viscous sheet model

We investigate in Sections 6 and 7 a three dimensional model of a thin viscous sheet over a fluid substrate and its two dimensional asymptotic limit.

We first present in Section 6 the three dimensional partial differential equations governing a thin viscous layer of an incompressible fluid with two free boundaries, an upper fluid/gas boundary and a lower fluid/substrate boundary. The upper gas may depend on a particular application under concern and will be denoted by 'gas' for the sake of notational simplicity. On the other hand, the fluid substrate will be modeled by using the hydrostatic approximation. In Section 7 we will perform an asymptotic analysis and derive the Saint-Venant equations with an energy equation and temperature dependent transport coefficients from the three dimensional governing equations presented in this section.

There are various examples of such viscous layers over fluid substrates as for instance oil slicks over water [19] float glasses [35], and atlantic waters over the deeper denser Mediterranean sea in the Strait of Gibraltar [31].

During the spreading of an oil spill, there exist indeed several regimes where it can be modeled as a thin viscous sheet over a water substrate [34]. This is notably the case during the gravity/viscous or viscous/surface-tension spreading regimes [19]. The incompressible oil flow then presents two free



Figure 1: Schematic of the thin viscous sheet

boundaries, the upper oil/air interface and the lower oil/sea interface. More refined models may also include other effects like wind dispersion, water currents, shore deposition, evaporation, or dissolution, in order to describe more realistically oil slick trajectories [34].

In a float glass, molten glass is flowing and floating above molten tin, and is progressively cooled in order to produced plate glass [35, 20, 21]. This procedure gives the glass sheet a smooth interface and modern windows are made from float glasses. The incompressible molten glass flow then presents two free boundaries, the upper glass/gas interface and the lower glass/tin interface. The reducing atmosphere above the molten glass and the tin bath is typically a mixture of nitrogen and hydrogen to prevent the oxidation of tin.

On the other hand, in the Strait of Gibtraltar, the denser Mediterranean sea flows below Atlandic waters penetrating in the Alboran sea. These phenomena may be modeled by using bi-layer Saint-Venant shallow water equations [31]. More recently, multi-layer Saint-Venant equations have also been investigated [26, 31, 1, 2].

Nevertheless, we will not discuss a particular application in the following sections since the models investigated may be applied to quite different situations. We will thus generically denote by 'fluid' the liquid constitutive of the viscous sheet, by 'gas' the gas above the sheet, and by 'substrate' or 'fluid substrate' the liquid substrate below the sheet.

### 6.1 Setting of the problem

We consider a three dimensional flow governed by the incompressible Navier-Stokes equations with temperature dependent transport coefficients. The flow configuration is depicted in Figure 1 with an upper fluid/gas free boundary and a lower fluid/substrate free boundary. The incompressible fluid constitutive of the viscous sheet is termed the 'fluid', the gas above the viscous sheet is termed the 'gas', and the lower fluid constitutive of the substrate is termed the 'substrate' or the 'fluid substrate'.

The equations governing the viscous incompressible fluid can be written in the non conservative form  $\partial_{\bf x} \cdot {\bf v} = 0,$ 

$$\begin{split} \rho \partial_t \mathbf{v} &+ \rho \mathbf{v} \cdot \boldsymbol{\partial}_{\mathbf{x}} \mathbf{v} + \boldsymbol{\partial}_{\mathbf{x}} \mathbf{p} - \boldsymbol{\partial}_{\mathbf{x}} \cdot (\eta \mathbf{d}) = \rho \mathbf{g}, \\ \rho c_v \partial_t T &+ \rho c_v \mathbf{v} \cdot \boldsymbol{\partial}_{\mathbf{x}} T - \boldsymbol{\partial}_{\mathbf{x}} \cdot (\lambda T) = \frac{1}{2} \eta \mathbf{d} : \mathbf{d}, \end{split}$$

where  $\partial_{\mathbf{x}} = (\partial_x, \partial_y, \partial_z)^t$  is the three dimensional gradient vector,  $\rho$  the constant density of the incompressible fluid,  $\mathbf{v} = (u, v, w)^t$  the three dimensional velocity vector,  $\mathbf{p}$  the pressure of the three dimensional glass flow,  $\mathbf{g} = (0, 0, \mathbf{g})^t$  the gravity assumed to be constant and vertical,  $\mathbf{d} = \partial_{\mathbf{x}} \mathbf{v} + \partial_{\mathbf{x}} \mathbf{v}^t$ the strain tensor,  $c_v$  the heat capacity per unit mass of the incompressible fluid,  $\eta$  the fluid viscosity and  $\lambda$  the fluid thermal conductivity of the fluid. We denote by  $(\mathbf{e}_x, \mathbf{e}_y, \mathbf{e}_z)$  the canonical basis vectors associated with the three dimensional cartesian coordinates  $\mathbf{x} = (x, y, z)^t$ . We will denote by  $\mathbf{\Pi} = -\eta \mathbf{d}$ the viscous tensor,  $\mathbf{P}$  the pressure tensor  $\mathbf{P} = \mathbf{pI} + \mathbf{\Pi}$ ,  $\boldsymbol{\sigma} = -\mathbf{P}$  the Cauchy stress tensor, and  $\mathbf{Q}$  the heat flux  $\mathbf{Q} = -\lambda \partial_{\mathbf{x}} T$ . Note that we use italic fonts in order to denote the asymptotic two dimensional Saint-Venant model and roman fonts in order to denote the original three dimensional incompressible Navier-Stokes model. We will assume in the following that the pressure in the fluid is measured relative to the atmospheric pressure  $\mathbf{p}_{\text{atm}}$  for the sake of simplicity.

The boundary conditions are that of free boundaries at the upper fluid/gas interface  $z = h_{gas}$  and at the lower fluid/substrate interface  $z = h_{sub}$ . On the top boundary, the fluid particles stay on the surface  $z - h_{gas} = 0$  and the usual kinematic condition yields that

$$w = \partial_t h_{\text{gas}} + u \partial_x h_{\text{gas}} + v \partial_y h_{\text{gas}},$$

where we have denoted by  $\mathbf{v} = (u, v, w)^t$  the three components of the velocity vector  $\mathbf{v}$ . On the other hand, the dynamic condition at the top free boundary can be written

$$\boldsymbol{\sigma} \cdot \mathbf{n}_{\mathrm{gas}} = \boldsymbol{\sigma}_{\mathrm{gas}} \cdot \mathbf{n}_{\mathrm{gas}} - \gamma_{\mathrm{f/g}} \mathcal{C}_{\mathrm{gas}} \mathbf{n}_{\mathrm{gas}},$$

where  $\gamma_{f/g}$  is the surface tension between the fluid and gas and  $C_{gas}$  the total curvature of the surface  $z = h_{gas}$  seen from the fluid and given by

$$\mathcal{C}_{\text{gas}} = \frac{\partial_x^2 h_{\text{gas}} \left(1 + (\partial_y h_{\text{gas}})^2\right) + \partial_y^2 h_{\text{gas}} (1 + (\partial_x h_{\text{gas}})^2) - 2\partial_x h_{\text{gas}} \partial_y h_{\text{gas}} \partial_{xy}^2 h_{\text{gas}}}{\left(1 + (\partial_x h_{\text{gas}})^2 + (\partial_y h_{\text{gas}})^2\right)^{3/2}}.$$

In this dynamic boundary condition, the outward normal vector at the fluid/gas interface is given by

$$\mathbf{n}_{\text{gas}} = \left( (\partial_x h_{\text{gas}})^2 + (\partial_y h_{\text{gas}})^2 + 1 \right)^{-1/2} (-\partial_x h_{\text{gas}}, -\partial_y h_{\text{gas}}, 1)^t,$$

and the stress tensor in gas by

$$\sigma_{\rm gas} \cdot \mathbf{n}_{\rm gas} = -p_{\rm atm} \mathbf{n}_{\rm gas},$$

where  $p_{atm}$  denotes the atmospheric pressure.

**Remark 6.1.** A more general dynamic boundary condition taking into account the spatial variations of the surface tension  $\gamma_{f/g}$  can be written in the form

$$m{\sigma}\cdot\mathbf{n}_{ ext{gas}} = m{\sigma}_{ ext{gas}}\cdot\mathbf{n}_{ ext{gas}} - \gamma_{ ext{f/g}}\mathcal{C}_{ ext{gas}}\mathbf{n}_{ ext{gas}} - (m{I}-\mathbf{n}_{ ext{gas}}\otimes\mathbf{n}_{ ext{gas}})m{\partial}_{m{x}}\gamma_{ ext{f/g}},$$

where  $\partial_x \gamma_{f/g}$  denotes the gradient of the surface tension  $\gamma_{f/g}$ . However, for the sake of simplicity, we will assume in the following that  $\gamma_{f/g}$  is a constant.

Similarly, at the lower boundary,  $z = h_{sub}$ , the vertical velocity component w is given by

$$w = \partial_t h_{\rm sub} + u \partial_x h_{\rm sub} + v \partial_y h_{\rm sub},$$

and the dynamic condition reads

$$\boldsymbol{\sigma} \cdot \mathbf{n}_{\mathrm{sub}} = \boldsymbol{\sigma}_{\mathrm{sub}} \cdot \mathbf{n}_{\mathrm{sub}} - \gamma_{\mathrm{f/s}} \mathcal{C}_{\mathrm{sub}} \mathbf{n}_{\mathrm{sub}},$$

where  $\gamma_{f/s}$  is the surface tension between the fluid and the substrate,  $C_{sub}$  the total curvature of the surface  $z = h_{sub}$  seen from the fluid, and

$$\mathbf{n}_{\mathrm{sub}} = \left( (\partial_x h_{\mathrm{sub}})^2 + (\partial_y h_{\mathrm{sub}})^2 + 1 \right)^{-1/2} (\partial_x h_{\mathrm{sub}}, \partial_y h_{\mathrm{sub}}, -1)^t,$$

the outward unit normal vector at the fluid/substrate interface. Thanks to the hydrostatic approximation, the normal component of the stress tensor in the fluid substrate is given by

$$\sigma_{\rm sub} \cdot \mathbf{n}_{\rm sub} = -\mathbf{p}_{\rm sub} \mathbf{n}_{\rm sub},$$

where  $p_{sub}$  denotes the pressure in the substrate flow given by

$$p_{sub} = p_{atm} + \rho_{sub}gh_{sub}.$$

From a thermal point of view, at the top and bottom interfaces, we have the boundary conditions

$$\begin{split} &-\lambda \partial_{\boldsymbol{x}} T \cdot \mathbf{n}_{\text{gas}} = \lambda^*_{\text{gas}} (T - T_{\text{gas}}), \\ &-\lambda \partial_{\boldsymbol{x}} T \cdot \mathbf{n}_{\text{sub}} = \lambda^*_{\text{sub}} (T - T_{\text{sub}}), \end{split}$$

where  $T_{\text{gas}}$  and  $T_{\text{sub}}$  are given temperatures in the gas and in the substrate flows, respectively, and where  $\lambda_{\text{gas}}^*$  and  $\lambda_{\text{sub}}^*$  are the heat exchange coefficients.

## 6.2 Rescaled equations

In order to perform an asymptotic analysis of the three dimensional incompressible fluid flow, we need to specify the order of magnitude of the various terms appearing in the governing equations. To this purpose, for each quantity  $\phi$ , we introduce a typical order of magnitude denoted by  $\langle \phi \rangle$ . We introduce in particular a characteristic horizontal length  $\langle x \rangle = \langle y \rangle$  and vertical length  $\langle z \rangle = \epsilon \langle x \rangle$  where the aspect ratio  $\epsilon$  is the small parameter associated with the thickness of the fluid viscous sheet. We correspondingly introduce a characteristic horizontal velocity  $\langle u \rangle = \langle v \rangle$  and vertical velocity  $\langle w \rangle = \epsilon \langle u \rangle$  as well as a characteristic density  $\langle \rho \rangle = \rho$  where  $\rho$  is the constant density of the fluid constitutive of the viscous sheet. Denoting by  $\langle \eta \rangle$  a characteristic viscosity, the Reynolds number Re is then given by

$$\operatorname{Re} = \frac{\langle \rho \rangle \langle u \rangle \langle x \rangle}{\langle \eta \rangle}.$$
(6.1)

We define the characteristic time from the characteristic length  $\langle x \rangle$  and the characteristic velocity  $\langle u \rangle$  by letting  $\langle t \rangle = \langle x \rangle / \langle u \rangle$ . Denoting by  $\langle c_v \rangle$  a typical heat capacity and  $\langle \lambda \rangle$  a characteristic heat conductivity of the fluid, the characteristic internal energy is defined by  $\langle e \rangle = \langle c_v \rangle \langle T \rangle$  and the Prandtl number Pr by

$$\Pr = \frac{\langle \eta \rangle \langle c_v \rangle}{\langle \lambda \rangle}.$$
(6.2)

Note that  $c_p = c_v$  for an incompressible fluid and that we may set for instance  $\langle c_v \rangle = R/m$  where R is the perfect gas constant and m the molar mass of the incompressible fluid. We will also denote by Ec the energy ratio or Eckert number

$$\operatorname{Ec} = \frac{\langle u \rangle^2}{\langle c_v \rangle \langle T \rangle}.$$
(6.3)

For a fluid, this number plays a similar rôle as that of the square of the Mach number for a gas. From these definitions we obtain that  $\langle \eta \rangle = \langle \rho \rangle \langle u \rangle \langle x \rangle / \text{Re}$ ,  $\langle e \rangle = \langle c_v \rangle \langle T \rangle = \langle u \rangle^2 / \text{Ec}$  and  $\langle \lambda \rangle = \langle \rho \rangle \langle u \rangle \langle x \rangle \langle c_v \rangle / (\text{RePr})$ . We define the characteristic pressure as  $\langle p \rangle = \langle \rho \rangle \langle u \rangle^2$  and the Froude number by

$$Fr = \frac{\langle u \rangle^2}{\langle g \rangle \langle x \rangle},\tag{6.4}$$

so that  $\langle g \rangle = \langle u \rangle^2 / (Fr \langle x \rangle)$ . Denoting by  $\langle \gamma \rangle$  a typical surface tension, the capilary number is defined by

$$Ca = \frac{\langle \eta \rangle \langle u \rangle}{\langle \gamma \rangle},\tag{6.5}$$

so that  $\langle \gamma \rangle = \langle x \rangle \langle \rho \rangle \langle u \rangle^2 / \text{ReCa.}$  We also introduce a typical heat exchange coefficient  $\langle \lambda^* \rangle$  and the reduced quantity

$$Ex = \frac{\langle \lambda^* \rangle \langle x \rangle}{\langle \lambda \rangle}.$$
(6.6)

In the asymptotic analysis, performed in the next section, it will be assumed that

$$\operatorname{Fr} = \epsilon \overline{\operatorname{Fr}}, \qquad \operatorname{Ca} = \frac{\overline{\operatorname{Ca}}}{\epsilon}, \qquad \operatorname{Ex} = \epsilon \overline{\operatorname{Ex}}, \tag{6.7}$$

and that the numbers Re, Pr, Ec,  $\overline{\text{Fr}}$ ,  $\overline{\text{Ca}}$ , and  $\overline{\text{Ex}}$  are of zeroth order with respect to  $\epsilon$ , that is, are finite as  $\epsilon \to 0$ . Assuming that  $\overline{\text{Ex}}$  and  $1/\overline{\text{Ca}}$  are small means that surface tension effects as well as thermal exchanges are corrective effects. In order to simplify the formal presentation, it will be convenient to define the modified reduced quantities

$$\overline{\eta} = \frac{\widehat{\eta}}{\text{Re}}, \qquad \overline{\lambda} = \frac{\widehat{\lambda}}{\text{PrRe}},$$
(6.8)

$$\overline{\mathbf{g}} = \frac{\widehat{\mathbf{g}}}{\overline{\mathrm{Fr}}}, \qquad \overline{\gamma} = \frac{\widehat{\gamma}}{\mathrm{Re}\overline{\mathrm{Ca}}}, \qquad \overline{\lambda}^* = \frac{\widehat{\lambda}^* \overline{\mathrm{Ex}}}{\mathrm{PrRe}}.$$
 (6.9)

These quantities are such that

$$\gamma = \epsilon < \rho > < u >^2 < x > \overline{\gamma}, \qquad g = < u >^2 \overline{g} / < x >, \tag{6.11}$$

$$\lambda^* = \epsilon < \rho > < u > < c_v > \overline{\lambda}^*, \tag{6.12}$$

and will simplify the formal presentation of the asymptotic analysis. From the aspect ratio of the thin viscous sheet, we also deduce that the curvature is typically of the order  $\langle C \rangle = \epsilon/\langle x \rangle$ . We will also denote by a the density ratio

$$\mathbf{a} = \frac{\rho}{\rho_{\rm sub}},\tag{6.13}$$

where  $\rho$  is the density of the incompressible fluid constitutive of the viscous sheet and  $\rho_{sub}$  the density of the incompressible substrate fluid.

**Remark 6.2.** Typical values for density ratios are  $a \simeq 0.70-0.97$  between crude oil and water for oil slicks,  $a \simeq 0.35$  between glass and tin for float glasses,  $a \simeq 0.997$  between Atlantic and Mediterranean waters. Typical aspect ratios are  $\epsilon \simeq 10^{-9}-10^{-6}$  for oil slicks. and  $\epsilon \simeq 10^{-3}$  for float glasses.

Upon defining the reduced quantity  $\hat{\phi} = \phi/\langle \phi \rangle$  associated with each quantity  $\phi$  of the fluid model, we can now estimate the order of magnitude of each term in the governing partial differential equations. Using the general notation for rescaled variables the reduced equations can be written in the form

$$\partial_{\widehat{\mathbf{x}}} \cdot \widehat{\mathbf{v}} = 0, \tag{6.14}$$

$$\partial_{\widehat{t}}\widehat{\mathbf{v}} + \widehat{\mathbf{v}} \cdot \partial_{\widehat{\mathbf{x}}}\widehat{\mathbf{v}} + \partial_{\widehat{\mathbf{x}}}\widehat{\mathbf{p}} - \partial_{\widehat{\mathbf{x}}} \cdot (\overline{\eta}\mathbf{d}) = \overline{\mathbf{g}},\tag{6.15}$$

$$\widehat{c}_v \partial_{\widehat{\mathbf{x}}} \widehat{T} + \widehat{c}_v \widehat{\mathbf{v}} \cdot \partial_{\widehat{\mathbf{x}}} \widehat{T} - \partial_{\widehat{\mathbf{x}}} \cdot (\overline{\lambda} \widehat{T}) = \overline{\Phi}, \tag{6.16}$$

where  $\overline{\Phi} = \frac{1}{2}\overline{\eta} \widehat{\mathbf{d}}: \widehat{\mathbf{d}}/\text{Ec}$  is the reduced viscous dissipation term. In order to perform an asymptotic expansion of all the flow variables, it is further necessary to explicit the governing equations in the horizontal and vertical directions. Upon expanding the flow vector equations and dividing the vertical momentum equation by the aspect ratio  $\epsilon$  we obtain that

$$\partial_{\widehat{x}}\widehat{u} + \partial_{\widehat{y}}\widehat{v} + \partial_{\widehat{z}}\widehat{w} = 0, \tag{6.17}$$

$$\partial_{\widehat{t}}\widehat{u} + \widehat{u}\,\partial_{\widehat{x}}\widehat{u} + \widehat{v}\,\partial_{\widehat{y}}\widehat{u} + \widehat{w}\,\partial_{\widehat{z}}\widehat{u} - \partial_{\widehat{x}}\left(2\overline{\eta}\partial_{\widehat{x}}\widehat{u}\right) \\ - \partial_{\widehat{y}}\left(\overline{\eta}(\partial_{\widehat{y}}\widehat{u} + \partial_{\widehat{x}}\widehat{v})\right) - \frac{1}{\epsilon^2}\partial_{\widehat{z}}\left(\overline{\eta}\partial_{\widehat{z}}\widehat{u}\right) - \partial_{\widehat{z}}\left(\overline{\eta}\partial_{\widehat{x}}\widehat{w}\right) + \partial_{\widehat{x}}\widehat{p} = 0,$$
(6.18)

$$\partial_{\widehat{t}}\widehat{v} + \widehat{u}\,\partial_{\widehat{x}}\widehat{v} + \widehat{v}\,\partial_{\widehat{y}}\widehat{v} + \widehat{w}\,\partial_{\widehat{z}}\widehat{v} - \partial_{\widehat{x}}\left(\overline{\eta}(\partial_{\widehat{y}}\widehat{u} + \partial_{\widehat{x}}\widehat{v})\right) \\ - \partial_{\widehat{y}}\left(2\overline{\eta}\partial_{\widehat{y}}\widehat{u}\right) - \frac{1}{\epsilon^{2}}\partial_{\widehat{z}}\left(\overline{\eta}\partial_{\widehat{z}}\widehat{v}\right) - \partial_{\widehat{z}}\left(\overline{\eta}\partial_{\widehat{y}}\widehat{w}\right) + \partial_{\widehat{y}}\widehat{p} = 0,$$
(6.19)

$$\partial_{\widehat{t}}\widehat{w} + \widehat{u}\,\partial_{\widehat{x}}\widehat{w} + \widehat{v}\,\partial_{\widehat{y}}\widehat{w} + \widehat{w}\,\partial_{\widehat{z}}\widehat{w} - \partial_{\widehat{x}}\left(\overline{\eta}\partial_{\widehat{x}}\widehat{w}\right) - \frac{1}{\epsilon^2}\partial_{\widehat{x}}\left(\overline{\eta}\partial_{\widehat{z}}\widehat{u}\right) - \partial_{\widehat{y}}\left(2\overline{\eta}\partial_{\widehat{y}}\widehat{w}\right) - \frac{1}{\epsilon^2}\partial_{\widehat{y}}\left(\overline{\eta}\partial_{\widehat{z}}\widehat{v}\right) - \frac{1}{\epsilon^2}\partial_{\widehat{z}}\left(2\overline{\eta}\partial_{\widehat{z}}\widehat{w}\right) + \frac{1}{\epsilon^2}\partial_{\widehat{z}}\widehat{p} = \frac{1}{\epsilon^2}\overline{g},$$
(6.20)

and

$$\widehat{c}_{v}\partial_{\widehat{t}}\widehat{T} + \widehat{c}_{v}\widehat{u}\,\partial_{\widehat{x}}\widehat{T} + \widehat{c}_{v}\widehat{v}\,\partial_{\widehat{y}}\widehat{T} + \widehat{c}_{v}\widehat{w}\,\partial_{\widehat{z}}\widehat{T} - \partial_{\widehat{x}}\left(\overline{\lambda}\partial_{\widehat{x}}\widehat{T}\right) 
- \partial_{\widehat{y}}\left(\overline{\lambda}\partial_{\widehat{y}}\widehat{T}\right) - \frac{1}{\epsilon^{2}}\partial_{\widehat{z}}\left(\overline{\lambda}\partial_{\widehat{z}}\widehat{T}\right) = \overline{\Phi},$$
(6.21)

where the reduced viscous dissipation  $\overline{\Phi}$  is given by

$$\overline{\Phi} = \frac{1}{2}\overline{\eta}\operatorname{Ec}\left(4(\partial_{\widehat{x}}\widehat{u})^2 + 4(\partial_{\widehat{y}}\widehat{v})^2 + 4(\partial_{\widehat{z}}\widehat{w})^2 + 2(\partial_{\widehat{y}}\widehat{u} + \partial_{\widehat{x}}\widehat{v})^2 + 2(\frac{1}{\epsilon}\partial_{\widehat{z}}\widehat{v} + \epsilon\partial_{\widehat{y}}\widehat{w})^2 + 2(\epsilon\partial_{\widehat{x}}\widehat{w} + \frac{1}{\epsilon}\partial_{\widehat{z}}\widehat{u})^2\right).$$
(6.22)

**Remark 6.3.** The internal energy per unit mass can also be written  $e = e^{\text{st}} + \int_{T^{\text{st}}}^{T} c_v(\tau) d\tau$  and the total energy per unit mass is given by  $e^{\text{tot}} = e + \frac{1}{2} \mathbf{v} \cdot \mathbf{v}$ . The reduced total energy per unit mass  $\hat{e}^{\text{tot}}$  can also be written  $\hat{e}^{\text{tot}} = \hat{e}^{\text{st}} + \int_{\hat{T}^{\text{st}}}^{\hat{T}} \hat{c}_v(\tau) d\tau + \frac{1}{2} \text{Ec}(\hat{u}^2 + \hat{v}^2 + \epsilon^2 \hat{w}^2)$ .

## 6.3 Rescaled boundary conditions

Upon using the general notation associated with rescaled variables the reduced kinematic boundary condition at the top rescaled free boundary  $\hat{z} - \hat{h}_{gas} = 0$  can be written

$$\widehat{w} = \partial_{\widehat{t}}\widehat{h}_{\text{gas}} + \widehat{u}\partial_{\widehat{x}}\widehat{h}_{\text{gas}} + \widehat{v}\partial_{\widehat{y}}\widehat{h}_{\text{gas}},$$

whereas the dynamic condition reads

$$\widehat{m{\sigma}} \cdot \widehat{m{n}}_{ ext{gas}} = \widehat{m{\sigma}}_{ ext{gas}} \cdot \widehat{m{n}}_{ ext{gas}} - \epsilon^2 \overline{\gamma}_{ ext{f/g}} \widehat{\mathcal{C}}_{ ext{gas}} \widehat{m{n}}_{ ext{gas}}$$

where

$$\widehat{\mathbf{n}}_{\text{gas}} = \left( (\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{gas}})^2 + (\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{gas}})^2 + 1 \right)^{-1/2} (-\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{gas}}, -\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{gas}}, 1)^t,$$

and where the normal component of the stress tensor in gas reads

,

$$\widehat{\boldsymbol{\sigma}}_{\text{gas}} \cdot \widehat{\mathbf{n}}_{\text{gas}} = -\widehat{\mathbf{p}}_{\text{atm}} \widehat{\mathbf{n}}_{\text{gas}}.$$

By decomposing the dynamic boundary condition componentwise, we obtain the three equations

$$\epsilon \widehat{\mathbf{p}} \partial_{\widehat{x}} \widehat{h}_{\text{gas}} + \widehat{\eta} \Big( 2 \partial_{\widehat{x}} \widehat{u} (-\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{gas}}) + (\partial_{\widehat{y}} \widehat{u} + \partial_{\widehat{x}} \widehat{v}) (-\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{gas}}) + \frac{1}{\epsilon} \partial_{\widehat{z}} \widehat{u} + \epsilon \partial_{\widehat{x}} \widehat{w} \Big) = \epsilon^3 \overline{\gamma}_{\text{f/g}} \widehat{\mathcal{C}}_{\text{gas}} \partial_{\widehat{x}} \widehat{h}_{\text{gas}},$$
(6.23)

$$\epsilon \widehat{\mathbf{p}} \partial_{\widehat{y}} \widehat{h}_{\text{gas}} + \widehat{\eta} \Big( (\partial_{\widehat{y}} \widehat{u} + \partial_{\widehat{x}} \widehat{v}) (-\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{gas}}) + 2 \partial_{\widehat{y}} \widehat{v} (-\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{gas}}) + \frac{1}{\epsilon} \partial_{\widehat{z}} \widehat{v} + \epsilon \partial_{\widehat{y}} \widehat{w} \Big) = \epsilon^3 \overline{\gamma}_{\text{f/g}} \widehat{\mathcal{C}}_{\text{gas}} \partial_{\widehat{y}} \widehat{h}_{\text{gas}},$$
(6.24)

$$-\widehat{\mathbf{p}} + \widehat{\eta} \Big( (\epsilon \partial_{\widehat{x}} \widehat{w} + \frac{1}{\epsilon} \partial_{\widehat{z}} \widehat{u}) (-\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{gas}}) + (\epsilon \partial_{\widehat{y}} \widehat{w} + \frac{1}{\epsilon} \partial_{\widehat{z}} \widehat{v}) (-\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{gas}}) + 2 \partial_{\widehat{z}} \widehat{w} \Big) = -\epsilon^2 \overline{\gamma}_{\text{f/g}} \widehat{\mathcal{C}}_{\text{gas}},$$
(6.25)

where the reduced curvature  $\widehat{\mathcal{C}}_{gas}$  can be written

$$\widehat{\mathcal{C}}_{\text{gas}} = \frac{\partial_{\widehat{x}}^2 \widehat{h}_{\text{gas}} \left(1 + \epsilon^2 (\partial_{\widehat{y}} \widehat{h}_{\text{gas}})^2\right) + \partial_{\widehat{y}}^2 \widehat{h}_{\text{gas}} (1 + \epsilon^2 (\partial_{\widehat{x}} \widehat{h}_{\text{gas}})^2\right) - 2\epsilon^2 \partial_{\widehat{x}} \widehat{h}_{\text{gas}} \partial_{\widehat{y}} \widehat{h}_{\text{gas}} \partial_{\widehat{x}\widehat{y}} \widehat{h}_{\text{gas}}}{\left(1 + \epsilon^2 (\partial_{\widehat{x}} \widehat{h}_{\text{gas}})^2 + \epsilon^2 (\partial_{\widehat{y}} \widehat{h}_{\text{gas}})^2\right)^{3/2}}.$$
(6.26)

Similarly, at the reduced free boundary  $\hat{z} - \hat{h}_{sub} = 0$  between the fluid and the substrate we can write that

$$\widehat{w} = \partial_{\widehat{t}} h_{\rm sub} + \widehat{u} \partial_{\widehat{x}} h_{\rm sub} + \widehat{v} \partial_{\widehat{y}} h_{\rm sub},$$

and the dynamic condition reads

$$\widehat{oldsymbol{\sigma}} \cdot \widehat{\mathbf{n}}_{ ext{sub}} = \widehat{oldsymbol{\sigma}}_{ ext{sub}} \cdot \widehat{\mathbf{n}}_{ ext{sub}} - \epsilon^2 \overline{\gamma}_{ ext{f/s}} \widehat{\mathcal{C}}_{ ext{sub}} \widehat{\mathbf{n}}_{ ext{sub}},$$

with

$$\widehat{\mathbf{n}}_{\mathrm{sub}} = \left( (\epsilon \partial_{\widehat{x}} \widehat{h}_{\mathrm{sub}})^2 + (\epsilon \partial_{\widehat{y}} \widehat{h}_{\mathrm{sub}})^2 + 1 \right)^{-1/2} (\epsilon \partial_{\widehat{x}} \widehat{h}_{\mathrm{sub}}, \epsilon \partial_{\widehat{y}} \widehat{h}_{\mathrm{sub}}, -1)^t$$

The normal component of the stress tensor in the fluid substrate reads

$$\widehat{\boldsymbol{\sigma}}_{\mathrm{sub}}\cdot\widehat{\mathbf{n}}_{\mathrm{sub}}=-\widehat{\mathbf{p}}_{\mathrm{sub}}\widehat{\mathbf{n}}_{\mathrm{sub}},$$

where  $\widehat{p}_{sub}$  is assumed to be hydrostatic. The dynamic vector boundary condition can be decomposed componentwise and yields that

$$-\epsilon \widehat{p}\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub}} + \widehat{\eta}\Big(2\partial_{\widehat{x}}\widehat{u}(\epsilon\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub}}) + (\partial_{\widehat{y}}\widehat{u} + \partial_{\widehat{x}}\widehat{v})(\epsilon\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub}}) - \frac{1}{\epsilon}\partial_{\widehat{z}}\widehat{u} - \epsilon\partial_{\widehat{x}}\widehat{w}\Big) = -\frac{1}{\mathsf{a}}\widehat{h}_{\mathrm{sub}}\overline{g}(\epsilon\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub}}) - \epsilon^{3}\overline{\gamma}_{\mathrm{f/s}}\widehat{\mathcal{C}}_{\mathrm{sub}}\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub}},$$

$$(6.27)$$

$$-\epsilon \widehat{p}\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub}} + \widehat{\eta}\Big((\partial_{\widehat{y}}\widehat{u} + \partial_{\widehat{x}}\widehat{v})(\epsilon\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub}}) + 2\partial_{\widehat{y}}\widehat{v}(\epsilon\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub}}) - \frac{1}{\epsilon}\partial_{\widehat{z}}\widehat{v} - \epsilon\partial_{\widehat{y}}\widehat{w}\Big) = -\frac{1}{\mathsf{a}}\widehat{h}_{\mathrm{sub}}\overline{\mathsf{g}}(\epsilon\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub}}) - \epsilon^{3}\overline{\gamma}_{\mathrm{f/s}}\widehat{\mathcal{C}}_{\mathrm{sub}}\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub}},$$

$$(6.28)$$

$$\widehat{\mathbf{p}} + \widehat{\eta} \Big( \big( \frac{1}{\epsilon} \partial_{\widehat{z}} \,\widehat{u} + \epsilon \partial_{\widehat{x}} \,\widehat{w} \big) \big( \epsilon \partial_{\widehat{x}} \,\widehat{h}_{\mathrm{sub}} \big) + \big( \frac{1}{\epsilon} \partial_{\widehat{z}} \,\widehat{v} + \epsilon \partial_{\widehat{y}} \,\widehat{w} \big) \big( \epsilon \partial_{\widehat{y}} \,\widehat{h}_{\mathrm{sub}} \big) \\ - 2 \partial_{\widehat{z}} \,\widehat{w} \Big) = \frac{1}{\mathsf{a}} \widehat{h}_{\mathrm{sub}} \overline{\mathbf{g}} + \epsilon^2 \overline{\gamma}_{\mathrm{f/s}} \widehat{\mathcal{C}}_{\mathrm{sub}}.$$
(6.29)

Finally, the rescaled thermal boundary conditions at the top and bottom interfaces, are in the form

$$\begin{split} -\overline{\lambda} \; & \frac{-\partial_{\widehat{x}} \widehat{T}(\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{gas}}) - \partial_{\widehat{y}} \widehat{T}(\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{gas}}) + \frac{1}{\epsilon} \partial_{\widehat{z}} \widehat{T}}{\left((\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{gas}})^2 + (\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{gas}})^2 + 1\right)^{1/2}} = \epsilon \overline{\lambda}_{\text{gas}}^* (\widehat{T} - \widehat{T}_{\text{gas}}), \\ -\overline{\lambda} \; & \frac{\partial_{\widehat{x}} \widehat{T}(\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{sub}}) + \partial_{\widehat{y}} \widehat{T}(\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{sub}}) - \frac{1}{\epsilon} \partial_{\widehat{z}} \widehat{T}}{\left((\epsilon \partial_{\widehat{x}} \widehat{h}_{\text{sub}})^2 + (\epsilon \partial_{\widehat{y}} \widehat{h}_{\text{sub}})^2 + 1\right)^{1/2}} = \epsilon \overline{\lambda}_{\text{sub}}^* (\widehat{T} - \widehat{T}_{\text{sub}}), \end{split}$$

where  $\hat{T}_{gas}$  and  $\hat{T}_{sub}$  are the rescaled given temperatures in gas and in the substrate flow respectively, and where  $\overline{\lambda}_{gas}^*$  and  $\overline{\lambda}_{sub}^*$  are the rescaled heat exchange coefficients.

## 7 Derivation of the Saint-Venant equations

The governing equations presented in Section 2 and investigated in Sections 3–5 are now derived from an asymptotic analysis of the three dimensional incompressible equations modeling thin viscous sheets over fluid substrates presented in Section 6.

Asymptotic expansions are a powerful tool for deriving governing equations of multiscale medias. We refer in particular to the monographs of Milton Van Dyke [43] for asymptotic methods in fluid mechanics, Sanchez-Palencia [37] and Benssousan, Lions, and Papanicolaou [4] for asymptotic expansions in homogenization theory. In the context of thin viscous sheets over fluid substrates we mention in particular Howell [20, 21] who investigated isothermal flows. Gerbeau and Perthame have revisited the derivation and validated the Saint-Venant model by a direct numerical comparison with the underlying incompressible model [13]. Audusse et al have also recently investigated mutilayer media [1, 2].

The two-dimensional Saint-Venant system of partial differential equations with an energy equation and temperature dependent transport coefficient will be obtained as the zeroth order limit of the three dimentional incompressible model presented in Section 6. We remind that, in the asymptotic limit, the fluid parameters Re, Pr, Ec, Fr, Ca, and Ex are assumed to be of zeroth order with respect to  $\epsilon$ . The quantities associated with the three dimensional incompressible model are generally denoted by roman fonts whereas the quantities associated with the Saint-Venant two dimensional asymptotic limit will be denoted with math italic fonts. The pressure in the three dimensional flow is denoted by p for instance wheras it will be denoted by p in the two dimensional Saint-Venant limit model.

#### 7.1 Asymptotic expansions

In order to derive the Saint-Venant equations modeling thin viscous sheets over a fluid substrate from the three dimensional fluid equations described in Section 6, we expand in powers of the small parameter  $\epsilon^2$  the fluid variables

$$\widehat{u} = \widehat{u}_0 + \epsilon^2 \widehat{u}_2 + \mathcal{O}(\epsilon^4), \tag{7.1}$$

$$\widehat{v} = \widehat{v}_0 + \epsilon^2 \widehat{v}_2 + \mathcal{O}(\epsilon^4), \tag{7.2}$$

$$\widehat{w} = \widehat{w}_0 + \epsilon^2 \widehat{w}_2 + \mathcal{O}(\epsilon^4), \tag{7.3}$$

$$\widehat{T} = \widehat{T}_0 + \epsilon^2 \widehat{T}_2 + \mathcal{O}(\epsilon^4).$$
(7.4)

We also expand the free boundaries  $h_{gas}$  and  $h_{sub}$  and we define

$$h(t, x, y) = h_{gas}(t, x, y) - h_{sub}(t, x, y),$$
(7.5)

in such a way that

$$\widehat{h} = \widehat{h}_0 + \epsilon^2 \widehat{h}_2 + \mathcal{O}(\epsilon^4), \tag{7.6}$$

$$\widehat{h}_{\text{gas}} = \widehat{h}_{\text{gas0}} + \epsilon^2 \widehat{h}_{\text{gas2}} + \mathcal{O}(\epsilon^4), \tag{7.7}$$

$$\widehat{h}_{\rm sub} = \widehat{h}_{\rm sub0} + \epsilon^2 \widehat{h}_{\rm sub2} + \mathcal{O}(\epsilon^4).$$
(7.8)

Note that, after some algebra, only the factor  $\epsilon^2$  appears in the rescaled equations presented in the previous Sections 6.2–6.3. The asymptotic expansions (7.1)–(7.8) in terms of  $\epsilon^2$  are thus natural as they are in the small Mach number limit [14].

## 7.2 Zeroth order terms and compressibility

The terms of order  $\epsilon^{-2}$  in the  $\hat{u}$  and  $\hat{v}$  governing equations first yield that

$$\begin{aligned} \partial_{\widehat{z}}(\overline{\eta}_0 \partial_{\widehat{z}} \, \widehat{u}_0) &= 0, \\ \partial_{\widehat{z}}(\overline{\eta}_0 \partial_{\widehat{z}} \, \widehat{v}_0) &= 0, \end{aligned}$$

 $\overline{\eta}_0 = \overline{\eta}(\widehat{T}_0).$ 

where

These relations show that  $\overline{\eta}_0 \partial_{\widehat{z}} \widehat{u}_0$  and  $\overline{\eta}_0 \partial_{\widehat{z}} \widehat{v}_0$  are constants. However, the  $\epsilon^{-1}$  terms in the dynamic boundary conditions at the fluid/gas and fluid/substrate interfaces yield that  $\partial_{\widehat{z}} \widehat{u}_0 = 0$  and  $\partial_{\widehat{z}} \widehat{v}_0 = 0$  at both interfaces. We thus deduce that  $\partial_{\widehat{z}} \widehat{u}_0 = 0$  and  $\partial_{\widehat{z}} \widehat{v}_0 = 0$  for all  $\widehat{z}$  in such a way that

$$\hat{u}_0 = \hat{u}_0(\hat{t}, \hat{x}, \hat{y}),$$
$$\hat{v}_0 = \hat{v}_0(\hat{t}, \hat{x}, \hat{y}).$$

Similarly, the energy conservation equation yields at order  $\epsilon^{-2}$  that

$$-\partial_{\widehat{z}}(\overline{\lambda}_0\partial_{\widehat{z}}\widehat{T}_0) = \overline{\eta}_0\big((\partial_{\widehat{z}}\widehat{u}_0)^2 + (\partial_{\widehat{z}}\widehat{v}_0)^2\big),$$

where

$$\overline{\lambda}_0 = \overline{\lambda}(\widehat{T}_0),$$

in such a way that  $\partial_{\widehat{z}}(\overline{\lambda}_0\partial_{\widehat{z}}\widehat{T}_0) = 0$  since  $\partial_{\widehat{z}}\widehat{u}_0 = 0$  and  $\partial_{\widehat{z}}\widehat{v}_0 = 0$ . Since the  $\epsilon^{-1}$  terms of the thermal boundary conditions yield that  $\overline{\lambda}_0\partial_{\widehat{z}}\widehat{T}_0 = 0$  at both the fluid/gas and fluid/substrate interfaces, we again conclude that  $\partial_{\widehat{z}}\widehat{T}_0 = 0$  for all  $\widehat{z}$  in such a way that

$$\widehat{T}_0 = \widehat{T}_0(\widehat{t}, \widehat{x}, \widehat{y}).$$

This shows that  $\hat{h}_0$ ,  $\hat{u}_0$ ,  $\hat{v}_0$ , and  $\hat{T}_0$ —and incidentally  $\overline{\eta}_0$  and  $\overline{\lambda}_0$ —only depend on  $(\hat{t}, \hat{x}, \hat{y})$ , and  $\hat{h}_0$ ,  $\hat{u}_0$ ,  $\hat{v}_0$ , and  $\hat{T}_0$  will constitute the variables of the resulting Saint-Venant two dimensional model. We will also denote by  $\hat{v}_0$  the two-dimensional velocity vector  $\hat{v}_0 = (\hat{u}_0, \hat{v}_0)^t$ .

On the other hand, from the incompressibility equation at zeroth order we obtain that

$$\partial_{\widehat{z}}\widehat{w}_0 = -(\partial_{\widehat{x}}\widehat{u}_0 + \partial_{\widehat{y}}\widehat{v}_0),$$

so that  $\partial_{\widehat{z}} \widehat{w}_0$  is independent of  $\widehat{z}$ . This shows that  $\widehat{w}_0$  is an affine function of  $\widehat{z}$  and that

$$\widehat{w}_0(\widehat{t},\widehat{x},\widehat{y},\widehat{h}_{\text{gas}0}) - \widehat{w}_0(\widehat{t},\widehat{x},\widehat{y},\widehat{h}_{\text{sub}0}) = -(\partial_{\widehat{x}}\widehat{u}_0 + \partial_{\widehat{y}}\widehat{v}_0)(\widehat{h}_{\text{gas}0} - \widehat{h}_{\text{sub}0})$$

From the zeroth order kinematic conditions at  $\hat{z} = \hat{h}_{sub0}$  and  $\hat{z} = \hat{h}_{sub0}$  we next deduce that

$$\partial_{\widehat{t}}(\widehat{h}_{\text{gas0}} - \widehat{h}_{\text{sub0}}) + \widehat{u}_0 \partial_{\widehat{x}}(\widehat{h}_{\text{gas0}} - \widehat{h}_{\text{sub0}}) + \widehat{v}_0 \partial_{\widehat{y}}(\widehat{h}_{\text{gas0}} - \widehat{h}_{\text{sub0}}) = -(\partial_{\widehat{x}}\widehat{u}_0 + \partial_{\widehat{y}}\widehat{v}_0)(\widehat{h}_{\text{gas0}} - \widehat{h}_{\text{sub0}}),$$
(7.9)

which finally yields that

$$\partial_{\widehat{t}}\widehat{h}_0 + \partial_{\widehat{x}}(\widehat{h}_0\widehat{u}_0) + \partial_{\widehat{y}}(\widehat{h}_0\widehat{v}_0) = 0.$$
(7.10)

We have thus obtained a compressible model where the zeroth order height  $\hat{h}_0$  plays the rôle of a density.

## 7.3 Zeroth order pressure

From the zeroth order terms of the normal momentum conservation equation (6.20) we next obtain that

$$\partial_{\widehat{x}}(\overline{\eta}_0 \partial_{\widehat{z}} \widehat{u}_0) - \partial_{\widehat{y}}(\overline{\eta}_0 \partial_{\widehat{z}} \widehat{v}_0) - 2\partial_{\widehat{z}}(\overline{\eta}_0 \partial_{\widehat{z}} \widehat{w}_0) + \partial_{\widehat{z}} \widehat{p}_0 = \overline{g}_0,$$

but since  $\partial_{\widehat{z}} \widehat{u}_0 = 0$ ,  $\partial_{\widehat{z}} \widehat{v}_0 = 0$ ,  $\partial_{\widehat{z}} \overline{\eta}_0 = 0$ , and  $\partial_{\widehat{z}}^2 \widehat{w}_0 = 0$ , we deduce from this relation that

$$\partial_{\widehat{z}}\widehat{\mathbf{p}}_0 = \overline{\mathbf{g}}_0.$$

This shows that the pressure is hydrostatic since

$$\overline{\mathbf{g}}_0 = \overline{\mathbf{g}} = \mathrm{Cte},$$

where  $\overline{\mathbf{g}} = \overline{\mathbf{g}}_0 = (0, 0, \overline{g}_0)^t$  and  $\overline{g}_0$  is negative. The relation  $\partial_{\widehat{z}} \widehat{p}_0 = \overline{g}_0$  implies that

$$\widehat{\mathbf{p}}_0(\widehat{t},\widehat{x},\widehat{y},\widehat{z}) = \widehat{\mathbf{p}}_0(\widehat{t},\widehat{x},\widehat{y},\widehat{h}_{\mathrm{gas0}}) + \overline{\mathbf{g}}_0(\widehat{z}-\widehat{h}_{\mathrm{gas0}}),$$

but the third component of the dynamic condition at the fluid/gas interface also yields at zeroth order that  $-\hat{p}_0 + 2\overline{\eta}_0 \partial_{\hat{z}} \hat{w}_0 = 0$  at  $\hat{z} = \hat{h}_{gas0}$  in such a way that

$$\widehat{\mathbf{p}}_0(\widehat{t},\widehat{x},\widehat{y},\widehat{z}) = 2\overline{\eta}_0\partial_{\widehat{z}}\widehat{w}_0 + \overline{\mathbf{g}}_0(\widehat{z}-\widehat{h}_{\mathrm{gas}0})$$

On the other hand, the dynamic condition at zeroth order at the fluid/substrate interface gives  $-\hat{p}_0 + 2\bar{\eta}_0\partial_{\hat{z}}\hat{w}_0 = -\frac{1}{a}\hat{h}_{sub0}\bar{g}_0$  at  $\hat{z} = \hat{h}_{sub0}$  so that

$$\widehat{\mathbf{p}}_0(\widehat{t},\widehat{x},\widehat{y},\widehat{h}_{\mathrm{gas0}}) - \widehat{\mathbf{p}}_0(\widehat{t},\widehat{x},\widehat{y},\widehat{h}_{\mathrm{sub0}}) = -\frac{1}{\mathsf{a}}\widehat{h}_{\mathrm{sub0}}\overline{\mathbf{g}}_0,$$

and since the pressure at zeroth order is hydrostatic we also have

$$\widehat{\mathrm{p}}_{0}(\widehat{t},\widehat{x},\widehat{y},\widehat{h}_{\mathrm{gas0}}) - \widehat{\mathrm{p}}_{0}(\widehat{t},\widehat{x},\widehat{y},\widehat{h}_{\mathrm{sub0}}) = \overline{\mathrm{g}}_{0}(\widehat{h}_{\mathrm{gas0}} - \widehat{h}_{\mathrm{sub0}}).$$

We deduce from these relations that  $\hat{h}_0 = \hat{h}_{gas0} - \hat{h}_{sub0} = -\frac{1}{a}\hat{h}_{sub0}$  and finally that

$$\widehat{h}_{\text{gas0}} = (1 - \mathsf{a})\widehat{h}_0, \qquad \widehat{h}_{\text{sub0}} = -\mathsf{a}\widehat{h}_0.$$
(7.11)

These conditions (7.11) are easily interpreted as a an equilibrium condition above the substrate bath. Since the height of the outer free substrate bath is taken to be zero, we have of course  $\hat{h}_{gas0} > 0$  and  $\hat{h}_{sub0} < 0$ . Finally, since  $\partial_{\hat{x}} \hat{w}_0 = -(\partial_{\hat{x}} \hat{u}_0 + \partial_{\hat{y}} \hat{v}_0)$  and  $\hat{h}_{gas0} = (1 - a)\hat{h}_0$ , we have established that

$$\widehat{p}_{0}(\widehat{t},\widehat{x},\widehat{y},\widehat{z}) = -2\overline{\eta}_{0}(\partial_{\widehat{x}}\widehat{u}_{0} + \partial_{\widehat{y}}\widehat{v}_{0}) + \overline{g}_{0}(\widehat{z} - (1-\mathsf{a})\widehat{h}_{0}).$$
(7.12)

## 7.4 Zeroth order momentum equations

The horizontal momentum conservation equations at zeroth order yield

$$\partial_{\widehat{t}}\widehat{u}_0 + \widehat{u}_0\partial_{\widehat{x}}\widehat{u}_0 + \widehat{v}_0\partial_{\widehat{y}}\widehat{u}_0 - \partial_{\widehat{x}}(2\overline{\eta}_0\partial_{\widehat{x}}\widehat{u}_0) - \partial_{\widehat{y}}\left(\overline{\eta}_0(\partial_{\widehat{y}}\widehat{u}_0 + \partial_{\widehat{x}}\widehat{v}_0)\right) \\ - \partial_{\widehat{z}}(\overline{\eta}_0\partial_{\widehat{z}}\widehat{u}_2) - \partial_{\widehat{z}}(\overline{\eta}_0\partial_{\widehat{x}}\widehat{w}_0) + \partial_{\widehat{x}}\widehat{p}_0 = 0,$$
(7.13)

and

$$\partial_{\widehat{t}}\widehat{v}_0 + \widehat{u}_0\partial_{\widehat{x}}\widehat{v}_0 + \widehat{v}_0\partial_{\widehat{y}}\widehat{v}_0 - \partial_{\widehat{x}}\left(\overline{\eta}_0(\partial_{\widehat{y}}\widehat{u}_0 + \partial_{\widehat{x}}\widehat{v}_0)\right) - \partial_{\widehat{y}}(2\overline{\eta}_0\partial_{\widehat{y}}\widehat{v}_0) \\ - \partial_{\widehat{z}}(\overline{\eta}_0\partial_{\widehat{z}}\widehat{u}_2) - \partial_{\widehat{z}}(\overline{\eta}_0\partial_{\widehat{y}}\widehat{w}_0) + \partial_{\widehat{y}}\widehat{p}_0 = 0.$$

$$(7.14)$$

Integrating the first equation between  $\hat{h}_{sub0}$  and  $\hat{h}_{gas0}$  we obtain that

$$\hat{h}_{0}\left(\partial_{\widehat{t}}\widehat{u}_{0}+\widehat{u}_{0}\partial_{\widehat{x}}\widehat{u}_{0}+\widehat{v}_{0}\partial_{\widehat{y}}\widehat{u}_{0}-\partial_{\widehat{x}}(2\overline{\eta}_{0}\partial_{\widehat{x}}\widehat{u}_{0})\right)-\hat{h}_{0}\partial_{\widehat{y}}\left(\overline{\eta}_{0}(\partial_{\widehat{y}}\widehat{u}_{0}+\partial_{\widehat{x}}\widehat{v}_{0})\right)\\ -\overline{\eta}_{0}\left[\!\left[\partial_{\widehat{z}}\widehat{u}_{2}+\partial_{\widehat{x}}\widehat{w}_{0}\right]\!\right]+\int_{\widehat{h}_{\mathrm{sub0}}}^{\widehat{h}_{\mathrm{gas0}}}\!\!\!\!\!\!\partial_{\widehat{x}}\widehat{p}_{0}\,d\widehat{z}=0,$$

$$(7.15)$$

where, for any function  $\phi$  of  $(\hat{t}, \hat{x}, \hat{y}, \hat{z})$ , the bracket  $\llbracket \phi \rrbracket$  denotes the corresponding function of  $(\hat{t}, \hat{x}, \hat{y})$  defined by

$$\llbracket \phi \rrbracket (\hat{t}, \hat{x}, \hat{y}) = \phi (\hat{t}, \hat{x}, \hat{y}, \hat{h}_{\text{gas0}}(\hat{t}, \hat{x}, \hat{y})) - \phi (\hat{t}, \hat{x}, \hat{y}, \hat{h}_{\text{sub0}}(\hat{t}, \hat{x}, \hat{y})).$$
(7.16)

We now use the dynamic boundary condition at zeroth order in the x direction at both interfaces to get that

$$\begin{split} \widehat{\mathbf{p}}_{0}\partial_{\widehat{x}}\widehat{h}_{\mathrm{gas0}} &- 2\overline{\eta}_{0}\partial_{\widehat{x}}\widehat{u}_{0}\partial_{\widehat{x}}\widehat{h}_{\mathrm{gas0}} - \overline{\eta}_{0}(\partial_{\widehat{y}}\widehat{u}_{0} + \partial_{\widehat{x}}\widehat{v}_{0})\partial_{\widehat{y}}\widehat{h}_{\mathrm{gas0}} \\ &+ \overline{\eta}_{0}\partial_{\widehat{x}}\widehat{w}_{0} + \overline{\eta}_{0}\partial_{\widehat{z}}\widehat{u}_{2} = 0, \\ &- \widehat{\mathbf{p}}_{0}\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub0}} + 2\overline{\eta}_{0}\partial_{\widehat{x}}\widehat{u}_{0}\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub0}} + \overline{\eta}_{0}(\partial_{\widehat{y}}\widehat{u}_{0} + \partial_{\widehat{x}}\widehat{v}_{0})\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub0}} \\ &- \overline{\eta}_{0}\partial_{\widehat{x}}\widehat{w}_{0} - \overline{\eta}_{0}\partial_{\widehat{z}}\widehat{u}_{2} = \frac{\widehat{h}_{\mathrm{sub0}}}{\mathsf{a}}\overline{\mathbf{g}}_{0}\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub0}}. \end{split}$$

By adding these relations we deduce that

$$\overline{\eta}_{0} \llbracket \partial_{\widehat{z}} \widehat{u}_{2} + \partial_{\widehat{x}} \widehat{w}_{0} \rrbracket + \widetilde{p}_{0} \partial_{\widehat{x}} \widehat{h}_{0} - 2 \overline{\eta}_{0} \partial_{\widehat{x}} \widehat{u}_{0} \partial_{\widehat{x}} \widehat{h}_{0} - \overline{\eta}_{0} (\partial_{\widehat{y}} \widehat{u}_{0} + \partial_{\widehat{x}} \widehat{v}_{0}) \partial_{\widehat{y}} \widehat{h}_{0} = -\mathbf{a} \widehat{h}_{0} \overline{\mathbf{g}}_{0} \partial_{\widehat{x}} \widehat{h}_{0},$$
(7.17)

where

$$\widetilde{p}_0 = (1 - \mathsf{a})\widehat{p}_0(\widehat{t}, \widehat{x}, \widehat{y}, \widehat{h}_{\text{gas0}}) + \mathsf{a}\widehat{p}_0(\widehat{t}, \widehat{x}, \widehat{y}, \widehat{h}_{\text{sub0}}).$$
(7.18)

From the expression (7.12) of  $\hat{p}_0$  we obtain that

$$\widetilde{\mathbf{p}}_0 = -2\overline{\eta}_0(\partial_{\widehat{x}}\widehat{u}_0 + \partial_{\widehat{y}}\widehat{v}_0) - \overline{\mathbf{g}}_0 \mathbf{a}\widehat{h}_0, \tag{7.19}$$

so that

$$\overline{\eta}_{0} \llbracket \partial_{\widehat{x}} \widehat{u}_{2} + \partial_{\widehat{x}} \widehat{w}_{0} \rrbracket = 2 \overline{\eta}_{0} \partial_{\widehat{x}} \widehat{u}_{0} \partial_{\widehat{x}} \widehat{h}_{0} + \overline{\eta}_{0} (\partial_{\widehat{y}} \widehat{u}_{0} + \partial_{\widehat{x}} \widehat{v}_{0}) \partial_{\widehat{y}} \widehat{h}_{0} + 2 \overline{\eta}_{0} (\partial_{\widehat{x}} \widehat{u}_{0} + \partial_{\widehat{y}} \widehat{v}_{0}) \partial_{\widehat{x}} \widehat{h}_{0}.$$
(7.20)

Furthermore, we deduce from (7.12) that

$$\partial_{\widehat{x}}\widehat{\mathbf{p}}_0 = -\partial_{\widehat{x}} \left( 2\overline{\eta}_0 (\partial_{\widehat{x}}\widehat{u}_0 + \partial_{\widehat{y}}\widehat{v}_0) \right) - (1 - \mathsf{a})\partial_{\widehat{x}}\widehat{h}_0, \tag{7.21}$$

and  $\partial_{\hat{x}} \hat{p}_0$  is independent of  $\hat{z}$ . Combining (7.15)(7.20)(7.21), and since  $\partial_{\hat{x}} \hat{p}_0$  is independent of  $\hat{z}$ , we finally obtain that

$$\begin{aligned} \widehat{h}_{0} \Big( \partial_{\widehat{t}} \,\widehat{u}_{0} + \widehat{u}_{0} \partial_{\widehat{x}} \,\widehat{u}_{0} + \widehat{v}_{0} \partial_{\widehat{y}} \,\widehat{u}_{0} - \partial_{\widehat{x}} (2\overline{\eta}_{0} \partial_{\widehat{x}} \,\widehat{u}_{0}) \Big) &- \widehat{h}_{0} \partial_{\widehat{y}} \left( \overline{\eta}_{0} (\partial_{\widehat{y}} \,\widehat{u}_{0} + \partial_{\widehat{x}} \,\widehat{v}_{0}) \right) \\ &- 2\overline{\eta}_{0} (\partial_{\widehat{x}} \,\widehat{u}_{0} + \partial_{\widehat{y}} \,\widehat{v}_{0}) \partial_{\widehat{x}} \,\widehat{h}_{0} - 2\overline{\eta}_{0} \partial_{\widehat{x}} \,\widehat{u}_{0} \partial_{\widehat{x}} \,\widehat{h}_{0} - \overline{\eta}_{0} (\partial_{\widehat{y}} \,\widehat{u}_{0} + \partial_{\widehat{x}} \,\widehat{v}_{0}) \partial_{\widehat{y}} \,\widehat{h}_{0} \\ &+ \widehat{h}_{0} \Big( -\partial_{\widehat{x}} \Big( 2\overline{\eta}_{0} (\partial_{\widehat{x}} \,\widehat{u}_{0} + \partial_{\widehat{y}} \,\widehat{v}_{0}) \Big) - (1 - \mathsf{a}) \overline{\mathsf{g}}_{0} \partial_{\widehat{x}} \,\widehat{h}_{0} \Big) = 0. \end{aligned} \tag{7.22}$$

After some algebra this equation can be rewritten in the form

$$\widehat{h}_0 \partial_{\widehat{t}} \widehat{u}_0 + \widehat{h}_0 \widehat{u}_0 \partial_{\widehat{x}} \widehat{u}_0 + \widehat{h}_0 \widehat{v}_0 \partial_{\widehat{y}} \widehat{u}_0 - \partial_{\widehat{x}} (\widehat{h}_0 2 \overline{\eta}_0 \partial_{\widehat{x}} \widehat{u}_0) - \partial_{\widehat{y}} (\widehat{h}_0 \overline{\eta}_0 (\partial_{\widehat{y}} \widehat{u}_0 + \partial_{\widehat{x}} \widehat{v}_0)) - \partial_{\widehat{x}} (\widehat{h}_0 2 \overline{\eta}_0 (\partial_{\widehat{x}} \widehat{u}_0 + \partial_{\widehat{y}} \widehat{v}_0)) - \frac{1}{2} (1 - \mathsf{a}) \overline{g}_0 \partial_{\widehat{x}} \widehat{h}_0^2 = 0.$$

$$(7.23)$$

Using the compressibility equation (7.10) and defining the new pressure

$$\widehat{p}_0 = -\frac{1}{2}(1-\mathsf{a})\overline{g}_0\,\widehat{h}_0^2 = \frac{1}{2}(1-\mathsf{a})|\overline{g}_0|\,\widehat{h}_0^2,\tag{7.24}$$

not to be confused with  $\hat{p}_0$ , and defining the new viscous tensor

$$\overline{\Pi}_{0\widehat{x}\widehat{x}} = -\overline{\eta}_0\widehat{h}_0(4\partial_{\widehat{x}}\widehat{u}_0 + 2\partial_{\widehat{y}}\widehat{v}_0), \qquad \overline{\Pi}_{0\widehat{x}\widehat{y}} = -\overline{\eta}_0\widehat{h}_0(\partial_{\widehat{y}}\widehat{u}_0 + \partial_{\widehat{x}}\widehat{v}_0), \tag{7.25}$$

the equation governing  $\hat{u}_0$  is rewritten in the form

$$\partial_{\widehat{t}}(\widehat{h}_{0}\widehat{u}_{0}) + \partial_{\widehat{x}}(\widehat{h}_{0}\widehat{u}_{0}^{2}) + \partial_{\widehat{y}}(\widehat{h}_{0}\widehat{u}_{0}\widehat{v}_{0}) + \partial_{\widehat{x}}\overline{\Pi}_{0\widehat{x}\widehat{x}} + \partial_{\widehat{y}}\overline{\Pi}_{0\widehat{x}\widehat{y}} + \partial_{\widehat{x}}\widehat{p}_{0} = 0.$$
(7.26)

We can proceed similarly for the second horizontal momentum conservation equation which yields upon integration between  $\hat{h}_{sub0}$  and  $\hat{h}_{gas0}$  that

We now use the dynamic boundary condition at zeroth order in the y direction at both interfaces to get that

$$\begin{split} \widehat{\mathbf{p}}_{0}\partial_{\widehat{y}}\widehat{h}_{\mathrm{gas0}} &- \overline{\eta}_{0}(\partial_{\widehat{y}}\widehat{u}_{0} + \partial_{\widehat{x}}\widehat{v}_{0})\partial_{\widehat{x}}\widehat{h}_{\mathrm{gas0}} - 2\overline{\eta}_{0}\partial_{\widehat{y}}\widehat{v}_{0}\partial_{\widehat{y}}\widehat{h}_{\mathrm{gas0}} \\ &+ \overline{\eta}_{0}\partial_{\widehat{y}}\widehat{w}_{0} + \overline{\eta}_{0}\partial_{\widehat{z}}\widehat{v}_{2} = 0, \\ &- \widehat{\mathbf{p}}_{0}\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub0}} + \overline{\eta}_{0}(\partial_{\widehat{y}}\widehat{u}_{0} + \partial_{\widehat{x}}\widehat{v}_{0})\partial_{\widehat{x}}\widehat{h}_{\mathrm{sub0}} + 2\overline{\eta}_{0}\partial_{\widehat{y}}\widehat{v}_{0}\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub0}} \\ &- \overline{\eta}_{0}\partial_{\widehat{y}}\widehat{w}_{0} - \overline{\eta}_{0}\partial_{\widehat{z}}\widehat{v}_{2} = -\frac{\widehat{h}_{\mathrm{sub0}}}{\mathsf{a}}\overline{\mathbf{g}}_{0}\partial_{\widehat{y}}\widehat{h}_{\mathrm{sub0}}. \end{split}$$

By adding these relations we deduce that

$$\overline{\eta}_{0} \llbracket \partial_{\widehat{z}} \widehat{v}_{2} + \partial_{\widehat{y}} \widehat{w}_{0} \rrbracket + \widetilde{p}_{0} \partial_{\widehat{y}} \widehat{h}_{0} - \overline{\eta}_{0} (\partial_{\widehat{y}} \widehat{u}_{0} + \partial_{\widehat{x}} \widehat{v}_{0}) \partial_{\widehat{x}} \widehat{h}_{0} - 2 \overline{\eta}_{0} \partial_{\widehat{y}} \widehat{v}_{0} \partial_{\widehat{y}} \widehat{h}_{0} = -\mathbf{a} \widehat{h}_{0} \overline{\mathbf{g}}_{0} \partial_{\widehat{y}} \widehat{h}_{0},$$
(7.28)

so that from (7.18)

$$\overline{\eta}_{0} \llbracket \partial_{\widehat{z}} \widehat{v}_{2} + \partial_{\widehat{y}} \widehat{w}_{0} \rrbracket = \overline{\eta}_{0} (\partial_{\widehat{y}} \widehat{u}_{0} + \partial_{\widehat{x}} \widehat{v}_{0}) \partial_{\widehat{x}} \widehat{h}_{0} + 2 \overline{\eta}_{0} \partial_{\widehat{y}} \widehat{v}_{0} \partial_{\widehat{y}} \widehat{h}_{0} + 2 \overline{\eta}_{0} (\partial_{\widehat{x}} \widehat{u}_{0} + \partial_{\widehat{y}} \widehat{v}_{0}).$$
(7.29)

Furthermore, we deduce from (7.12) that

$$\partial_{\widehat{y}}\widehat{p}_0 = -\partial_{\widehat{y}} \left( 2\overline{\eta}_0 (\partial_{\widehat{x}}\widehat{u}_0 + \partial_{\widehat{y}}\widehat{v}_0) \right) - (1 - \mathsf{a})\partial_{\widehat{y}}\widehat{h}_0, \tag{7.30}$$

and  $\partial_{\hat{y}} \hat{p}_0$  is independent of  $\hat{z}$ . Combining (7.27)(7.29)(7.30), and since  $\partial_{\hat{y}} \hat{p}_0$  is independent of  $\hat{z}$ , we finally obtain that

$$\hat{h}_{0}\partial_{\widehat{t}}\widehat{v}_{0} + \hat{h}_{0}\widehat{u}_{0}\partial_{\widehat{x}}\widehat{v}_{0} + \hat{h}_{0}\widehat{v}_{0}\partial_{\widehat{y}}\widehat{v}_{0} - \partial_{\widehat{x}}\left(\hat{h}_{0}\overline{\eta}_{0}(\partial_{\widehat{y}}\widehat{u}_{0} + \partial_{\widehat{x}}\widehat{v}_{0})\right) - \partial_{\widehat{y}}\left(\hat{h}_{0}2\overline{\eta}_{0}\partial_{\widehat{y}}\widehat{v}_{0}\right) \\ - \partial_{\widehat{y}}\left(\hat{h}_{0}2\overline{\eta}_{0}(\partial_{\widehat{x}}\widehat{u}_{0} + \partial_{\widehat{y}}\widehat{v}_{0})\right) - \frac{1}{2}(1 - \mathsf{a})\overline{\mathsf{g}}_{0}\partial_{\widehat{y}}\widehat{h}_{0}^{2} = 0.$$

$$(7.31)$$

Defining

$$\overline{\Pi}_{0\widehat{y}\widehat{x}} = -\overline{\eta}_0\widehat{h}_0(\partial_{\widehat{y}}\widehat{u}_0 + \partial_{\widehat{x}}\widehat{v}_0), \qquad \overline{\Pi}_{0\widehat{y}\widehat{y}} = -\overline{\eta}_0\widehat{h}_0(2\partial_{\widehat{x}}\widehat{u}_0 + 4\partial_{\widehat{y}}\widehat{v}_0), \tag{7.32}$$

the equation governing  $\hat{v}_0$  is easily rewritten in the form

$$\partial_{\widehat{t}}(\widehat{h}_0\widehat{v}_0) + \partial_{\widehat{x}}(\widehat{h}_0\widehat{u}_0\widehat{v}_0) + \partial_{\widehat{y}}(\widehat{h}_0\widehat{v}_0^2) + \partial_{\widehat{x}}\overline{\Pi}_{0\widehat{y}\widehat{x}} + \partial_{\widehat{y}}\overline{\Pi}_{0\widehat{y}\widehat{y}} + \partial_{\widehat{y}}\widehat{p}_0 = 0.$$
(7.33)

Upon defining  $\widehat{\boldsymbol{v}}_0 = (\widehat{u}_0, \widehat{v}_0)^t$ ,  $\widehat{\boldsymbol{x}} = (\widehat{x}, \widehat{y})^t$ , and

$$\overline{\boldsymbol{\Pi}}_{0} = \begin{pmatrix} \overline{\boldsymbol{\Pi}}_{0\widehat{x}\widehat{x}} & \overline{\boldsymbol{\Pi}}_{0\widehat{x}\widehat{y}} \\ \overline{\boldsymbol{\Pi}}_{0\widehat{y}\widehat{x}} & \overline{\boldsymbol{\Pi}}_{0\widehat{y}\widehat{y}} \end{pmatrix},$$
(7.34)

both momentum equations can be rewritten in vector form

$$\partial_{\widehat{t}}(\widehat{h}_0\widehat{v}_0) + \partial_{\widehat{x}} \cdot \left(\widehat{h}_0\widehat{v}_0 \otimes \widehat{v}_0 + \widehat{p}_0 I\right) + \partial_{\widehat{x}} \cdot \overline{\Pi}_0 = 0, \tag{7.35}$$

in such a way that the height  $\hat{h}_0$  plays the rôle of a density and  $\hat{p}_0$  the rôle of a pressure for the two dimensional Saint-Venant model.

## 7.5 Zeroth order energy equation

Upon using  $\partial_{\hat{z}} \hat{u}_0 = \partial_{\hat{z}} \hat{v}_0 = \partial_{\hat{z}} \hat{T}_0 = \partial_{\hat{z}} \overline{\lambda}_0 = 0$ , the energy conservation equation at zeroth order yields that

$$\widehat{c}_{v0}\partial_{\widehat{t}}\widehat{T}_{0} + \widehat{c}_{v0}\widehat{u}_{0}\partial_{\widehat{x}}\widehat{T}_{0} + \widehat{c}_{v0}\widehat{v}_{0}\partial_{\widehat{y}}\widehat{T}_{0} - \partial_{\widehat{x}}\left(\overline{\lambda}_{0}\partial_{\widehat{x}}\widehat{T}_{0}\right) \\
- \partial_{\widehat{y}}\left(\overline{\lambda}_{0}\partial_{\widehat{y}}\widehat{T}_{0}\right) - \partial_{\widehat{z}}\left(\overline{\lambda}_{0}\partial_{\widehat{z}}\widehat{T}_{2}\right) = \overline{\Phi}_{0},$$
(7.36)

where the zeroth order viscous dissipation  $\overline{\Phi}_0$  is given by

$$\overline{\Phi}_0 = \frac{1}{2}\overline{\eta}_0 \operatorname{Ec}\left(4(\partial_{\widehat{x}}\widehat{u}_0)^2 + 4(\partial_{\widehat{y}}\widehat{v}_0)^2 + 4(\partial_{\widehat{x}}\widehat{u}_0 + \partial_{\widehat{y}}\widehat{v}_0)^2 + 2(\partial_{\widehat{y}}\widehat{u}_0 + \partial_{\widehat{x}}\widehat{v}_0)^2\right).$$
(7.37)

Integrating the equation (7.36) between  $\hat{h}_{sub0}$  and  $\hat{h}_{gas0}$  we obtain that

$$\widehat{h}_{0}\left(\widehat{c}_{v0}\partial_{\widehat{t}}\widehat{T}_{0}+\widehat{c}_{v0}\widehat{u}_{0}\partial_{\widehat{x}}\widehat{T}_{0}+\widehat{c}_{v0}\widehat{v}_{0}\partial_{\widehat{y}}\widehat{T}_{0}-\partial_{\widehat{x}}(\overline{\lambda}_{0}\partial_{\widehat{x}}\widehat{T}_{0})\right)-\widehat{h}_{0}\partial_{\widehat{y}}(\overline{\lambda}_{0}\widehat{T}_{0})$$

$$-\widehat{h}_{0}\overline{\Phi}_{0}-\overline{\lambda}_{0}\left[\!\left[\partial_{\widehat{z}}\widehat{T}_{2}\right]\!\right]=0.$$
(7.38)

We now use the thermal boundary condition at zeroth order at both interfaces to get that

$$\begin{aligned} &-\overline{\lambda}_0 \left( -\partial_{\widehat{x}} \widehat{T}_0 \partial_{\widehat{x}} \widehat{h}_{\text{gas0}} - \partial_{\widehat{y}} \widehat{T}_0 \partial_{\widehat{y}} \widehat{h}_{\text{gas0}} + \partial_{\widehat{z}} \widehat{T}_2 \right) = \overline{\lambda}_{0\text{gas}}^* (\widehat{T}_0 - \widehat{T}_{0\text{gas}}), \\ &-\overline{\lambda}_0 \left( \partial_{\widehat{x}} \widehat{T}_0 \partial_{\widehat{x}} \widehat{h}_{\text{sub0}} + \partial_{\widehat{y}} \widehat{T}_0 \partial_{\widehat{y}} \widehat{h}_{\text{sub0}} - \partial_{\widehat{z}} \widehat{T}_2 \right) = \overline{\lambda}_{0\text{sub}}^* (\widehat{T}_0 - \widehat{T}_{0\text{sub}}), \end{aligned}$$

By adding these equations we obtain that

$$-\overline{\lambda}_0 \llbracket \partial_{\widehat{x}} \widehat{T}_2 \rrbracket + \overline{\lambda}_0 \partial_{\widehat{x}} \widehat{T}_0 \partial_{\widehat{x}} \widehat{h}_0 + \overline{\lambda}_0 \partial_{\widehat{y}} \widehat{T}_0 \partial_{\widehat{y}} \widehat{h}_0 = \overline{\lambda}_0^* (\widehat{T}_0 - \widehat{T}_{0\text{mix}}),$$
(7.39)

where we have defined

$$\widehat{T}_{0\text{mix}} = \frac{\overline{\lambda}_{0\text{gas}}^* \widehat{T}_{0\text{gas}} + \overline{\lambda}_{0\text{sub}}^* \widehat{T}_{0\text{sub}}}{\overline{\lambda}_{0\text{gas}}^* + \overline{\lambda}_{0\text{sub}}^*},$$

and

$$\overline{\lambda}_0^* = \overline{\lambda}_{0\text{gas}}^* + \overline{\lambda}_{0\text{sub}}^*$$

Combining (7.38)(7.39) we obtain that

$$\hat{h}_{0}\left(\hat{c}_{v0}\partial_{\hat{t}}\hat{T}_{0}+\hat{c}_{v0}\hat{u}_{0}\partial_{\hat{x}}\hat{T}_{0}+\hat{c}_{v0}\hat{v}_{0}\partial_{\hat{y}}\hat{T}_{0}\right)-\partial_{\hat{x}}(\hat{h}_{0}\overline{\lambda}_{0}\partial_{\hat{x}}\hat{T}_{0})\right)\\-\partial_{\hat{y}}(\hat{h}_{0}\overline{\lambda}_{0}\hat{T}_{0})-\hat{h}_{0}\overline{\Phi}_{0}=-\overline{\lambda}_{0}^{*}(\hat{T}_{0}-\hat{T}_{0\mathrm{mix}}).$$
(7.40)

Furthemore, the dissipation term  $\hat{h}_0 \overline{\Phi}_0$  is easily rewritten in the form

$$\overline{h}_0 \overline{\Phi}_0 = -\mathrm{Ec} \overline{\boldsymbol{\Pi}}_0 : \boldsymbol{\partial}_{\widehat{\boldsymbol{x}}} \widehat{\boldsymbol{v}}_0.$$
(7.41)

Denoting the heat loss term by

$$\widehat{\mathcal{H}}_0 = -\overline{\lambda}_0^* (\widehat{T}_0 - \widehat{T}_{0\text{mix}}), \qquad (7.42)$$

the internal energy per unit mass by

$$\widehat{e}_0 = \widehat{e}^{\mathrm{st}} + \int_{\widehat{T}^{\mathrm{st}}}^{\widehat{T}_0} \widehat{c}_{v0}(\widehat{\tau}) \, d\widehat{\tau} + \frac{1}{2}(1-\mathsf{a})\mathrm{Ec}|\overline{\mathsf{g}}_0|\widehat{h}_0, \tag{7.43}$$

and the heat flux vector by

$$\overline{\boldsymbol{Q}}_0 = (\overline{\mathcal{Q}}_{0\widehat{x}}, \overline{\mathcal{Q}}_{0\widehat{y}})^t, \tag{7.44}$$

where

$$\overline{\mathcal{Q}}_{0\widehat{x}} = -\widehat{h}_0\overline{\lambda}_0\partial_{\widehat{x}}\widehat{T}_0, \qquad \overline{\mathcal{Q}}_{0\widehat{y}} = -\widehat{h}_0\overline{\lambda}_0\partial_{\widehat{y}}\widehat{T}_0, \tag{7.45}$$

the energy conservation equation is rewritten in the form

$$\widehat{h}_0 \partial_{\widehat{t}} \widehat{e}_0 + \widehat{h}_0 \widehat{v}_0 \cdot \partial_{\widehat{x}} \widehat{e}_0 + \partial_{\widehat{x}} \cdot \overline{Q}_0 + \operatorname{Ec} \widehat{p}_0 \partial_{\widehat{x}} \cdot \widehat{v}_0 + \operatorname{Ec} \overline{\Pi}_0 : \partial_{\widehat{x}} \widehat{v}_0 = \widehat{\mathcal{H}}_0.$$
(7.46)

Note that the inclusion of the term  $\frac{1}{2}(1-\mathbf{a})\operatorname{Ec}|\overline{g}_0|\hat{h}_0$  in the internal energy is associated with the pressure work term  $\operatorname{Ec}\hat{p}_0\partial_{\widehat{x}}\cdot\widehat{v}_0$  in the energy equation thanks to the relation  $\partial_{\widehat{t}}\hat{h}_0 + \widehat{v}_0\cdot\partial_{\widehat{x}}\hat{h}_0 + \hat{h}_0\partial_{\widehat{x}}\cdot\widehat{v}_0 = 0$ . Finally, upon multiplying the momentum governing equation by the velocity vector  $\widehat{v}_0$ , we obtain the kinetic energy governing equation, which can be multiplied by Ec and added to the internal energy governing equation in order to obtain the total energy conservation equation in the form

$$\partial_{\widehat{t}}(\widehat{h}_{0}\widehat{e}_{0}^{\text{tot}}) + \partial_{\widehat{x}} \cdot \left( (\widehat{h}_{0}\widehat{e}_{0}^{\text{tot}} + \operatorname{Ec}\widehat{p}_{0})\widehat{v}_{0} \right) + \partial_{\widehat{x}} \cdot (\overline{Q}_{0} + \operatorname{Ec}\overline{\Pi}_{0} \cdot \widehat{v}_{0}) = \widehat{\mathcal{H}}_{0},$$
(7.47)

where

$$\hat{e}_0^{\text{tot}} = \hat{e}_0 + \frac{1}{2} \text{Ec}(\hat{u}_0^2 + \hat{v}_0^2), \tag{7.48}$$

is the reduced total energy per unit mass.

## 7.6 Resulting model

From the previous sections, we can summarize the zeroth order rescaled governing equations in the form

$$\partial_{\widehat{t}}\widehat{h}_0 + \partial_{\widehat{x}} \cdot (\widehat{h}_0 \widehat{v}_0) = 0, \tag{7.49}$$

$$\partial_{\widehat{t}}(\widehat{h}_0\widehat{v}_0) + \partial_{\widehat{x}}\cdot \left(\widehat{h}_0\widehat{v}_0\otimes\widehat{v}_0 + \widehat{p}_0I\right) + \partial_{\widehat{x}}\cdot\overline{\Pi}_0 = 0, \tag{7.50}$$

$$\partial_{\widehat{t}}(\widehat{h}_0\widehat{e}_0^{\text{tot}}) + \partial_{\widehat{x}} \cdot \left( (\widehat{h}_0\widehat{e}_0^{\text{tot}} + \operatorname{Ec}\widehat{p}_0)\widehat{v}_0 \right) + \partial_{\widehat{x}} \cdot (\overline{Q}_0 + \operatorname{Ec}\overline{\Pi}_0 \cdot \widehat{v}_0) = \widehat{\mathcal{H}}_0.$$
(7.51)

The pressure  $\hat{p}_0$  is given by (7.24), the total energy  $\hat{e}_0^{\text{tot}}$  by (7.48), and internal energy  $\hat{e}_0$  by (7.43). The viscous tensor  $\overline{\Pi}_0$  is given by (7.25)(7.32), the heat flux  $\overline{Q}_0$  by (7.45) and the heat loss term  $\hat{\mathcal{H}}_0$  by (7.42).

Upon restoring the physical dimensions of the flow quantities  $t = \langle x \rangle \hat{t} / \langle u \rangle$ ,  $\boldsymbol{x} = \langle x \rangle \hat{\boldsymbol{x}}$ ,  $h_0 = \epsilon \langle x \rangle \hat{h}_0$ ,  $\boldsymbol{v}_0 = \langle u \rangle \hat{\boldsymbol{v}}_0$ ,  $p_0 = \langle h \rangle \langle u \rangle^2 \hat{p}_0$ ,  $e_0^{\text{tot}} = \langle c_v \rangle \langle T \rangle \hat{\boldsymbol{e}}_0^{\text{tot}}$ ,  $\boldsymbol{\Pi}_0 = \langle h \rangle \langle u \rangle^2 \boldsymbol{\Pi}_0$ ,  $\boldsymbol{Q}_0 = \langle h \rangle \langle u \rangle \langle c_v \rangle \langle T \rangle \boldsymbol{\Pi}_0$ , and  $\mathcal{H}_0 = \langle h \rangle \langle u \rangle \langle c_v \rangle \langle T \rangle \hat{\mathcal{H}}_0 / \langle x \rangle$ , we obtain after some algebra that

$$\partial_t h_0 + \partial_x \cdot (h_0 \boldsymbol{v}_0) = 0, \qquad (7.52)$$

$$\partial_t (h_0 \boldsymbol{v}_0) + \partial_{\boldsymbol{x}} \cdot \left( h_0 \boldsymbol{v}_0 \otimes \boldsymbol{v}_0 + p_0 \boldsymbol{I} \right) + \partial_{\boldsymbol{x}} \cdot \boldsymbol{\Pi}_0 = 0, \tag{7.53}$$

$$\partial_t (h_0 e_0^{\text{tot}}) + \partial_x \cdot \left( (h_0 e_0^{\text{tot}} + p_0) \boldsymbol{v}_0 \right) + \partial_x \cdot (\boldsymbol{Q}_0 + \boldsymbol{\Pi}_0 \cdot \boldsymbol{v}_0) = \mathcal{H}_0.$$
(7.54)

The scaled thermodynamic relations are

$$e_0^{\text{tot}} = e_0 + \frac{1}{2}(u_0^2 + v_0^2), \tag{7.55}$$

$$e_0 = e_0^{\rm st} + \int_{T_0^{\rm st}}^{T_0} (\tau) \, d\tau + \frac{1}{2} (1 - \mathsf{a}) |\mathbf{g}_0| h_0, \tag{7.56}$$

$$p_0 = \frac{1}{2}(1-\mathsf{a})|\mathbf{g}_0|h_0^2. \tag{7.57}$$

The scaled viscous tensor is given by

$$\boldsymbol{\Pi}_{0} = -\nu_{0}h_{0}\left(\boldsymbol{\partial}_{\boldsymbol{x}}\boldsymbol{v}_{0} + \boldsymbol{\partial}_{\boldsymbol{x}}\boldsymbol{v}_{0}^{t} + 2\boldsymbol{\partial}_{\boldsymbol{x}}\cdot\boldsymbol{v}_{0}\boldsymbol{I}\right) = \begin{pmatrix} \boldsymbol{\Pi}_{0xx} & \boldsymbol{\Pi}_{0xy} \\ \boldsymbol{\Pi}_{0yx} & \boldsymbol{\Pi}_{0yy} \end{pmatrix},$$
(7.58)

with

$$\begin{split} \Pi_{0xx} &= -\nu_0 h_0 (4\partial_x u_0 + 2\partial_y v_0), & \Pi_{0xy} &= -\nu_0 h_0 (\partial_y u_0 + \partial_x v_0), \\ \Pi_{0yx} &= -\nu_0 h_0 (\partial_y u_0 + \partial_x v_0), & \Pi_{0xy} &= -\nu_0 h_0 (2\partial_x u_0 + 4\partial_y v_0), \end{split}$$

where the kinematic viscosity is given by

$$\nu_0 = \frac{\eta(T_0)}{\rho}.$$
 (7.59)

Strictly speaking, only the quantity  $\rho \Pi_0/h_0$  is homogeneous to a viscous tensor and  $\Pi_0/h_0$  to a kinematic viscous tensor. Similarly, only the quantity  $\rho p_0/h_0$  is homogeneous to a pressure and  $p_0/h_0$  to a kinematic pressure. However, the multiplication by  $h_0$  is natural in a two dimensional context since then internal constraints arise through lines and not surfaces. Finally, the heat flux is given by

$$\boldsymbol{Q}_0 = (\mathcal{Q}_{0x}, \mathcal{Q}_{0y})^t = -\varkappa_0 h_0 (\partial_x T_0, \partial_y T_0)^t, \qquad (7.60)$$

where the kinematic thermal conductivity is given by

$$\varkappa_0 = \frac{\lambda(T_0)}{\rho}.\tag{7.61}$$

Strictly speaking, only the quantity  $\rho Q_0/h_0$  is homogeneous to a heat flux and  $Q_0/h_0$  to a kinematic heat flux. On the other hand, the heat loss term reads

$$\mathcal{H}_0 = -\frac{\lambda_0^*}{\rho} (T_0 - T_{0\text{mix}}), \tag{7.62}$$

where  $\lambda_0^* = \lambda_{0gas}^* + \lambda_{0sub}^*$  and

$$T_{0\rm mix} = \frac{\lambda_{0\rm gas}^* T_{0\rm gas} + \lambda_{0\rm sub}^* T_{0\rm sub}}{\lambda_{0\rm gas}^* + \lambda_{0\rm sub}^*}.$$
(7.63)

This model (7.52)-(7.63) is exactly the model that we have investigated in Sections 2–5 of this paper.



Figure 2: A local chart of the free boundary in the xy plane



Figure 3: Schematic of a slice of the thin viscous sheet free boundary

**Remark 7.1.** Saint-Venant models with a local energy partial differential equation should not be confused with isothermal models incorporating a global kinetic energy balance as investigated for instance by Kanayama [23].

#### 7.7 Boundary conditions

We present in this section typical free boundary conditions associated with thin viscous sheets over fluid substrates. These boundary conditions are written at the free boundary of the two-dimensional Saint-Venant model. These boundary conditions are not used in this paper and are only written here for completeness.

The two-dimensional Saint-Venant equations governing thin viscous sheets have been derived in the previous sections from the three dimensional incompressible Navier-Stokes equations governing incompressible fluids. Similarly, the boundary conditions associated with the two dimensional Saint-Venant model will be derived from the boundary conditions and conservation equations of the three dimensional model.

Exchanging eventually the rôle of x and y, we may assume that the free boundary can locally be written in the form  $x = X_{\rm b}(t, y)$ . The local geometry of such a free boundary  $x = X_{\rm b}(t, y)$  is depicted in Figure 2. The boundary conditions associated with the two dimensional Saint-Venant model at the free boundary  $x = X_{\rm b}(t, y)$  can be decomposed into a kinematic condition, a dynamic momentum boundary condition, and a thermal boundary condition.

We first investigate the dynamic momentum boundary condition at the free boundary. To this aim, we consider a slice of the free boundary of the three dimensional incompressible model in the plane spanned by  $\mathbf{n}_{\rm b}$  and  $\mathbf{e}_z$ , where  $\mathbf{n}_{\rm b}$  is the outward unit normal of the free boundary  $x = X_{\rm b}$  in the xy plane as depicted in Figure 2

$$\mathbf{n}_{\rm b} = \left(1 + (\partial_y X_{\rm b})^2\right)^{-1/2} \left(1, -\partial_y X_{\rm b}, 0\right)^t.$$
(7.64)

We next define  $\mathbf{e}_{\tilde{x}} = \mathbf{n}_{b}$  and  $\mathbf{e}_{\tilde{y}} = \mathbf{e}_{z} \wedge \mathbf{e}_{\tilde{x}}$  in such a way that  $\mathbf{e}_{\tilde{x}}, \mathbf{e}_{\tilde{y}}, \mathbf{e}_{z}$  form a direct orthonormal basis, and we denote by  $(\tilde{x}, \tilde{y}, z)$  the corresponding coordinates so that  $\tilde{x}$  is measured along  $\mathbf{n}_{b}$ . The geometry of the corresponding slice in the plane  $(\tilde{x}, z)$  of the free boundary associated with the threedimensional model is presented in Figure 3 where the fluid lay above the substrate. The asymptotic dynamic boundary condition is obtained upon integrating the horizontal momentum equation in the domain PQR. Since this domain is assumed to be of size  $\mathcal{O}(\epsilon^{2})$ , all inertial terms will be neglected in comparison with the force terms that are  $\mathcal{O}(\epsilon)$ . The forces acting on this volume are the surface tension forces, the viscous constraints on PR, and Archemedes' forces on QR. Note that we only consider the horizontal momentum equation so that there is no gravity term. Since the pressure in the substrate fluid is hydrostatic, and keeping in mind that all pressure are evaluated relative to the atmospheric pressure, the resultant of Archimedes forces on QR can be written

$$-\int_{QR} \rho_{\rm sub} g h_{\rm sub} \mathbf{n}_{\rm sub} \, d\tilde{s}_{\rm sub},$$

where  $\tilde{s}_{sub}$  is the arclength along the curve  $(\tilde{x}, \tilde{h}_{sub}(t, \tilde{x}, \tilde{y}))$ . In this expression, we have denoted  $\tilde{h}_{sub}(t, \tilde{x}, \tilde{y}) = h_{sub}(t, x, y)$  and  $\mathbf{n}_{sub}$  the corresponding outward oriented normal vector

$$\mathbf{n}_{\mathrm{sub}} = rac{\partial_{ ilde{x}} h_{\mathrm{sub}} \mathbf{n}_{\mathrm{b}} - \mathbf{e}_z}{\sqrt{1 + (\partial_{ ilde{x}} h_{\mathrm{sub}})^2}}.$$

Since the normal vector  $\mathbf{n}_{sub}$  is oriented downward the arc QR must be oriented from Q to R. The horizontal projection of this Archemedes' force is easily evaluated as

$$\int_{\mathbf{QR}} \rho_{\mathrm{sub}} \mathbf{g} h_{\mathrm{sub}} \mathbf{n}_{\mathrm{sub}} \cdot \mathbf{n}_{\mathrm{b}} \, d\tilde{s}_{\mathrm{sub}} = \frac{1}{2} \rho_{\mathrm{sub}} \mathbf{g} \left( h_{\mathrm{sub}}^2(\mathbf{Q}) - h_{\mathrm{sub}}^2(\mathbf{R}) \right), \tag{7.65}$$

since

$$\mathbf{n}_{\mathrm{sub}} \cdot \mathbf{n}_{\mathrm{b}} = \frac{\partial_{\tilde{x}} h_{\mathrm{sub}}}{\sqrt{1 + (\partial_{\tilde{x}} h_{\mathrm{sub}})^2}}, \qquad d\tilde{s}_{\mathrm{sub}} = -\sqrt{1 + (\partial_{\tilde{x}} h_{\mathrm{sub}})^2} \ d\tilde{x}.$$

On the other hand, the curvatures in the  $\tilde{x}$  direction are  $\mathcal{O}(1/\epsilon)$  whereas the curvatures in the  $\tilde{y}$  direction are  $\mathcal{O}(\epsilon)$ —and may be neglected—in such a way that the total curvatures  $\mathcal{C}_{gas}$  and  $\mathcal{C}_{sub}$  may be approximated as

$$\mathcal{C}_{\text{gas}} = \frac{\partial_{\tilde{x}}^2 h_{\text{gas}}}{\left(1 + (\partial_{\tilde{x}} h_{\text{gas}})^2\right)^{3/2}}, \qquad \mathcal{C}_{\text{sub}} = \frac{\partial_{\tilde{x}}^2 h_{\text{sub}}}{\left(1 + (\partial_{\tilde{x}} h_{\text{sub}})^2\right)^{3/2}}.$$
(7.66)

Using these expressions, the surface tension forces acting on PQR can be written

$$\int_{PQ} \partial_{\tilde{s}}(\gamma_{\rm f/g}\boldsymbol{\tau}_{\rm gas}) \, d\tilde{s}_{\rm gas} + \int_{QR} \partial_{\tilde{s}}(\gamma_{\rm f/s}\boldsymbol{\tau}_{\rm sub}) \, d\tilde{s}_{\rm sub},$$

where  $\tau_{\rm sub}$  is the tangent vector along the arc  $(\tilde{x}, \tilde{h}_{\rm sub}(t, \tilde{x}, \tilde{y}))$  oriented from Q to R, and  $\tilde{s}_{\rm gas}$  and  $\tau_{\rm gas}$  are the arclength and tangent vector along the arc  $(\tilde{x}, \tilde{h}_{\rm gas}(t, \tilde{x}, \tilde{y}))$  oriented from P to Q. We have used in particular the differential relations  $\partial_{\tilde{s}} \tau_{\rm gas} = C_{\rm gas} \mathbf{n}_{\rm gas}$  and  $\partial_{\tilde{s}} \tau_{\rm sub} = C_{\rm sub} \mathbf{n}_{\rm sub}$ . Furthermore, since  $\mathbf{n}_{\rm gas}$  is upward and the arc PQ oriented from P to Q, we may assume that at zeroth order  $\tau_{\rm gas}(P) = \mathbf{e}_{\tilde{x}} = \mathbf{n}_{\rm b}$ . Similarly, since  $\mathbf{n}_{\rm sub}$  is downward and the arc QR oriented from Q to R, we may assume that at zeroth order  $\tau_{\rm sub}(R) = -\mathbf{e}_{\tilde{x}} = -\mathbf{n}_{\rm b}$ . Integrating along the arcs PQ and QR, the surface tension forces are thus found to be

$$\gamma_{\mathrm{f/s}}(\boldsymbol{\tau}_{\mathrm{sub}}(\mathrm{R}) - \boldsymbol{\tau}_{\mathrm{sub}}(\mathrm{Q})) + \gamma_{\mathrm{f/g}}(\boldsymbol{\tau}_{\mathrm{gas}}(\mathrm{Q}) - \boldsymbol{\tau}_{\mathrm{gas}}(\mathrm{P})).$$

We now use the fundamental relation relating the tangent vectors at the triple-point Q

$$-\gamma_{\rm f/s}\boldsymbol{\tau}_{\rm sub}(\mathbf{Q}) + \gamma_{\rm f/g}\boldsymbol{\tau}_{\rm gas}(\mathbf{Q}) - \gamma_{\rm g/s}\boldsymbol{\tau}_{\rm ext}(\mathbf{Q}) = 0, \tag{7.67}$$

where  $z - h_{\text{ext}} = 0$  denotes the free surface between gas and the fluid substrate,  $\gamma_{\text{g/s}}$  the surface tension between gas and the fluid substrate, s a point as depicted on Figure 3,  $(\tilde{x}, \tilde{h}_{\text{ext}}(t, \tilde{x}, \tilde{y}))$  the arc qs oriented from Q to s, and  $\tau_{\text{ext}}$  the corresponding tangent vector. Since this arc is oriented from Q to s with  $\mathbf{n}_{\text{ext}}$  oriented upward, we may assume that at zeroth order  $\tau_{\text{ext}}(s) = \mathbf{e}_{\tilde{x}} = \mathbf{n}_{\text{b}}$ . This relation (7.67) can be used to simplify the expression of the surface tension forces by eliminating all quantities associated with the triple point Q, provided we can express the tangent vector  $\tau_{\text{ext}}(Q)$ . To this aim, we can use the dynamic equilibrium condition at the gas/substrate interface which states that

$$\boldsymbol{\sigma}_{\mathrm{sub}} \cdot \mathbf{n}_{\mathrm{ext}} = \boldsymbol{\sigma}_{\mathrm{gas}} \cdot \mathbf{n}_{\mathrm{ext}} - \mathcal{C}_{\mathrm{ext}} \gamma_{\mathrm{g/s}} \mathbf{n}_{\mathrm{ext}} = \boldsymbol{\sigma}_{\mathrm{gas}} \cdot \mathbf{n}_{\mathrm{ext}} - \partial_{\tilde{s}} (\gamma_{\mathrm{g/s}} \boldsymbol{\tau}_{\mathrm{ext}}), \tag{7.68}$$

where  $C_{\text{ext}}$  is the total curvature of the surface  $z = h_{\text{ext}}$  which may also be approximated as

$$C_{\text{ext}} = \frac{\partial_{\tilde{x}}^2 h_{\text{ext}}}{\left(1 + (\partial_{\tilde{x}} h_{\text{ext}})^2\right)^{3/2}}.$$
(7.69)

Using that the pressure is hydrostatic in the fluid substrate, we deduce from (7.68) that

$$\int_{\mathbf{Q}\mathbf{S}} \rho_{\text{sub}} \mathbf{g} h_{\text{ext}} \, \mathbf{n}_{\text{ext}} \, d\tilde{s}_{\text{ext}} + \gamma_{\text{g/s}} \big( \boldsymbol{\tau}_{\text{ext}}(\mathbf{Q}) - \boldsymbol{\tau}_{\text{ext}}(\mathbf{S}) \big) = 0$$

Eliminating the contributions associated with the triple point, the resulting horizontal force on the control volume PQR is found to be

$$\begin{split} \int_{\mathrm{PR}} & (\mathbf{p}\mathbf{I} - \eta \mathbf{d}) \cdot \mathbf{n}_{\mathrm{b}} \, dz - \mathbf{n}_{\mathrm{b}} \int_{\mathrm{QR}} \rho_{\mathrm{sub}} \mathbf{g} h_{\mathrm{sub}} \mathbf{n}_{\mathrm{sub}} \cdot \mathbf{n}_{\mathrm{b}} \, d\tilde{s}_{\mathrm{sub}} \\ & - \mathbf{n}_{\mathrm{b}} \int_{\mathrm{QS}} \rho_{\mathrm{sub}} \mathbf{g} h_{\mathrm{ext}} \mathbf{n}_{\mathrm{ext}} \cdot \mathbf{n}_{\mathrm{b}} \, d\tilde{s}_{\mathrm{ext}} - \mathbf{n}_{\mathrm{b}} (\gamma_{\mathrm{f/s}} + \gamma_{\mathrm{f/g}} - \gamma_{\mathrm{g/s}}) \end{split}$$

The horizontal projection of the surface tension force due to the substrate is easily evaluated as

$$\int_{\mathbf{QS}} \rho_{\mathrm{subg}} h_{\mathrm{ext}} \mathbf{n}_{\mathrm{ext}} \cdot \mathbf{n}_{\mathrm{b}} \, d\tilde{s}_{\mathrm{ext}} = \frac{1}{2} \rho_{\mathrm{subg}} \left( h_{\mathrm{ext}}^2(\mathbf{S}) - h_{\mathrm{ext}}^2(\mathbf{Q}) \right), \tag{7.70}$$

since

$$\mathbf{n}_{\text{ext}} \cdot \mathbf{n}_{\text{b}} = \frac{\partial_{\tilde{x}} h_{\text{ext}}}{\sqrt{1 + (\partial_{\tilde{x}} h_{\text{ext}})^2}}, \qquad d\tilde{s}_{\text{ext}} = \sqrt{1 + (\partial_{\tilde{x}} h_{\text{ext}})^2} \ d\tilde{x},$$

and we may chose that the vertical axis in such a way that  $h_{\text{ext}}(s) = 0$  since pressures are measured relative to the atmospheric pressure. Upon defining

$$\gamma = \frac{\gamma_{\rm g/s} - \gamma_{\rm f/s} - \gamma_{\rm f/g}}{\rho}.$$
(7.71)

and using the relations (7.65) and (7.70) the resulting horizontal force on the control volume PQR at zeroth order reads

$$\int_{\mathrm{PR}} (\mathbf{p}_0 \mathbf{I} - \eta_0 \mathbf{d}_0) \cdot \mathbf{n}_\mathrm{b} \, dz - \mathbf{n}_\mathrm{b} \left( \frac{1}{2} \rho_{\mathrm{sub}} |\mathbf{g}_0| h_{\mathrm{sub0}}^2(\mathbf{R}) + \rho \gamma \right). \tag{7.72}$$

Since the control volume PQR is of the order of  $\epsilon^2$ , we can neglect the inertial term and write that the resulting force (7.72) vanishes at zeroth order.

The zeroth order force  $\int_{PR} (p_0 \mathbf{I} - \eta_0 \mathbf{d}_0) \cdot \mathbf{n}_b dz$  can be evaluated from the expression of the zeroth order strain tensor  $\mathbf{d}_0$  and of the zeroth order pressure  $p_0$ . Since the second order tensor  $\mathbf{d}_0$  restricted to the plane spanned by  $\mathbf{e}_x$  and  $\mathbf{e}_y$  can be written  $\partial_x \mathbf{v}_0 + \partial_x \mathbf{v}_0^t$  and is independent of z we directly obtain upon integration that

$$\int_{\mathrm{PR}} \eta_0 \mathbf{d}_0 \cdot \mathbf{n}_{\mathrm{b}} \, dz = \eta_0 h_0 (\boldsymbol{\partial}_{\boldsymbol{x}} \boldsymbol{v}_0 + \boldsymbol{\partial}_{\boldsymbol{x}} \boldsymbol{v}_0^t) \cdot \mathbf{n}_{\mathrm{b}}.$$

On the other hand, from  $\mathbf{p}_0 = -2\eta_0(\partial_x u_0 + \partial_y v_0) + \mathbf{g}_0 z - (1 - \mathbf{a})\mathbf{g}_0 h_0$ , we obtain upon integration that

$$-\int_{\mathrm{PR}} \mathbf{p}_0 \, dz = 2\eta_0 h_0 (\partial_x u_0 + \partial_y v_0) + \frac{1}{2} \rho h_0^2 \mathbf{g}_0.$$

The last term  $\frac{1}{2}\rho h_0^2 g_0$  can then be combined with the contribution  $\frac{1}{2}\rho_{\rm sub}|g_0|h_{\rm ext}^2(\mathbf{R})$  from (7.72) to form the pressure term  $\rho p_0 = \frac{1}{2}\rho(1-\mathbf{a})g_0h_0^2$  of the two dimensional model. On the other hand, the term  $2\eta_0h_0(\partial_x u_0 + \partial_y v_0)$  will complete the isotropic part of  $\boldsymbol{\Pi}_0$ . Upon combining the above relations and dividing by the fluid density  $\rho$  we have finally established the dynamic boundary condition

$$-(p_0\mathbf{I}+\boldsymbol{\Pi}_0)\cdot\mathbf{n}_{\rm b}=\gamma\mathbf{n}_{\rm b}.\tag{7.73}$$

where  $\gamma = (\gamma_{g/s} - \gamma_{f/s} - \gamma_{f/g})/\rho$ .

**Remark 7.2.** It is interesting to note that in the zeroth order governing equations the surface tensions do not appear. Surface tensions only play a rôle in the zeroth order dynamic boundary conditions.

We can proceed similarly for the thermal boundary condition by considering the control domain PQR. We observe then that the heat exchange coefficients are of order  $\mathcal{O}(\epsilon)$  as are the length of the arcs PQ and QR in such a way that

$$\int_{PQ} \mathbf{Q}_0 \cdot \mathbf{n}_{gas} \, d\tilde{s}_{gas} = \int_{PQ} \lambda^*_{gas} (T_0 - T_{gas}) \, d\tilde{s}_{gas} = \mathcal{O}(\epsilon^2),$$

$$\int_{QR} \mathbf{Q}_0 \cdot \mathbf{n}_{sub} \, d\tilde{s}_{sub} = \int_{QR} \lambda_{sub}^* (T_0 - T_{sub}) \, d\tilde{s}_{sub} = \mathcal{O}(\epsilon^2),$$

where  $\mathbf{Q}_0 = -\lambda_0 \partial_{\mathbf{x}} T_0$  is the three dimensional zeroth order heat flux. Upon integrating the heat conservation equation in the domain PQR, we thus obtain at zeroth order that

$$\int_{PR} \lambda_0 \partial_x T_0 \cdot \mathbf{n}_b \, dz = 0,$$

$$\boldsymbol{Q}_0 \cdot \mathbf{n}_b = 0,$$
(7.74)

where  $Q_0 = -h_0 \lambda_0 \partial_x T_0$  is the zeroth order heat flux for the Saint-Venant model. Finally, since the free surface  $x = X_b(t, y)$  is a streamline of the two-dimensional flow model, we obtain the natural kinematic condition

$$u_0 = \partial_t X_{\rm b} + v_0 \partial_y X_{\rm b}.$$

This boundary condition can equivalently be obtained by integrating the incompressibility condition  $\partial_{\mathbf{x}} \cdot \mathbf{v} = 0$  on the control domain PQR. It is also easily rewritten in the coordinate independent form

$$(\boldsymbol{v}_0 - \boldsymbol{v}_b) \cdot \mathbf{n}_b = 0, \tag{7.75}$$

where  $\boldsymbol{v}_{\rm b} = \partial_t X_{\rm b}$  is the velocity of the free boundary and it is well known that the normal velocity  $\boldsymbol{v}_{\rm b} \cdot \mathbf{n}_{\rm b}$  is an intrinsic quantity associated with the free boundary.

The boundary conditions for the two-dimensional Saint-Venant model at the free boundary are finally constituted by the kinematic condition (7.75), the dynamic momentum boundary condition (7.73), and the thermal condition (7.74).

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and therefore

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